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# Analysis of Replacement of Internal Combustion Engine with the Hydrogen Fuel Cell in Ship Powertrain

Rafał Krakowski<sup>1\*</sup>

- <sup>1</sup> Faculty of Marine Engineering, Gdynia Maritime University, ul. Morska 81-87, 81-225 Gdynia, Poland
- \* Corrersponding author's e-mail: r.krakowski@wm.umg.edu.pl

# **ABSTRACT**

The article presents new propulsion concepts and related new energy sources of modern means of transportation. One of them is hydrogen fuel cells, widely regarded as one of the most promising and alternative solutions due mainly to their ecological nature. Also presented, the biggest problem associated with the development of fuel cells which is hydrogen. A huge energy input is used to produce it. In addition, the storage of hydrogen is highly problematic. With the introduction of increasingly stringent changes regarding toxic emissions into the atmosphere and the move toward emission-free transportation, the article examines the possibilities of converting a ship's reciprocating internal combustion engine propulsion system into an environmentally friendly one. In the rest of the article, legal aspects affecting the reduction of the environmental impact of exhaust emissions in the maritime industry are presented.Examples of fuel cell applications in current means of transportation are also discussed. In the main part of the article, the ship to be converted is presented, along with the planned voyage route. The main engine was converted to alternative electric motors, and a reduction gearbox in the main propulsion system was also selected. The power requirements for converting the ship's propulsion system were then determined. An inverter was selected to convert the generated direct current to alternating current and batteries to store the generated electricity. The final part of the article will analyse the feasibility of converting the propulsion of a Panamax-type bulk carrier with a piston internal combustion engine into an environmentally friendly propulsion system using a hydrogen fuel cell. The analysis will be carried out in terms of cost-effectiveness and technical feasibility. The article ended with conclusions.

**Keywords:** hydrogen fuel cell, unconventional energy sources, ECA zones, ship propulsion.

# **INTRODUCTION**

Nowadays there are various methods and means of transporting goods, but traditional sea transport is still used on a large scale. Sea transportation is not currently one of the fastest modes of transportation, but it is nevertheless very popular, mainly due to its relatively low prices. This is one of the most important advantages of this method of transporting cargo [1, 2]. Therefore, due to the growing popularity of this mode of transport, alternative propulsion systems are being sought that meet increasingly stringent regulations to protect the environment [3, 4].

Increasingly stringent environmental regulations and rising fuel prices have led to increasing attention to design and anticipated operating costs when designing new units and retrofitting older ones [5]. Besides, with the development of means of transport, new concepts of their propulsion systems and related new energy sources are being developed [6, 7]. Researchers around the world are working hard to implement new systems and technological solutions [8]. One of them is hydrogen fuel cells, which are now widely regarded as one of the most promising alternative solutions for decarbonising the maritime and world economies due to the possibility of replacement of fossil fuels [9, 10]. A fuel cell produces electricity from fuel supplied continuously. The power fuel is hydrogen, but the wide range of fuel cell capabilities also allows the use of fuel containing a large amount of this element, such as natural gas or even methanol [11, 12].

The biggest problem before the development of fuel cells is the fuel itself, namely hydrogen. Hydrogen is the fuel of the future, but a huge energy input is used to produce it. In addition, the storage of hydrogen itself is highly problematic, as hydrogen gas stores at a pressure of  $250 \div 700$  bar and it takes a huge amount of additional energy to store it. The second way is to store hydrogen in a liquid state at -240.18 °C (the critical temperature of hydrogen), but like the first way, it needs a large energy requirement to maintain its temperature [13, 14].

The average lifespan of a ship is between a dozen and several decades, and during such a period, increasingly stringent changes are being made regarding the emission of toxic compounds into the atmosphere. In order for a vessel to continue to perform its tasks in the changing reality, it must be constantly modernized and adapted to new conditions.

Accordingly, the purpose of the analysis presented in the article is to test the feasibility of converting the propulsion of a Panamax-type bulk carrier with a piston internal combustion engine into an environmentally friendly propulsion system using a hydrogen fuel cell. The analysis will be carried out in terms of cost-effectiveness and technical feasibility.

### **BACKGROUND**

### **Legal aspects**

Maritime shipping was, and still is today, fundamental to the proper functioning of the global economy. Comparing the maritime industry with alternative modes of transportation, the maritime industry has a relatively low impact on environmental pollution, but the impact is still noticeable and assessable in its effects.

Currently, the biggest issue for maritime organizations is the introduction of restrictions that will reduce greenhouse gas emissions. The big hope for shipowners who will have to comply with MARPOL is a nod to hydrogen as an alternative energy carrier.

For this reason, work and research are underway on the use of hydrogen fuel cells to propel ships, including seagoing vessels [16, 17].

The biggest advantage of a fuel cell is that it has high efficiency (depending on the type of fuel cell, up to 70%) and, what is important nowadays, low environmental harm.

Despite the progress of recent years, the maritime sector still relies almost entirely on fossil fuels and is a significant source of greenhouse gas emissions and other harmful pollutants. For this reason, a preliminary agreement has been signed on the decarbonization of the Fuel EU Maritime sector. The initiative is part of the "Ready for 55" package presented by the European Commission on July 14, 2021 [18, 19].

The intensity of greenhouse gas emissions from energy currently used on ships is to be reduced by promoting the use of cleaner renewable and low-emission fuels by ships calling at EU ports. In doing so, the smooth operation of maritime traffic and the non-disruption of the internal market are to be ensured [20].

### **Methods of producing hydrogen and their impact on the environment**

For hydrogen to successfully replace, or be one of the alternatives, there is a need to develop a cheap, fast and efficient method to produce it. Currently, 48% of hydrogen is produced by steam reforming of methane, 30% from oil, 18% from coal, and the remaining 4% from the electrolysis of water. The most well-known methods of obtaining hydrogen are: natural gas reforming, coal or coke gasification, plasma technology, water electrolysis, photo electrolysis and biological method [21, 22].

Metaphorically, the colors used to describe hydrogen carry information about how it is produced, the substrates and the energy sources used to obtain it. There are up to 7 distinguished categories/colors, but only three of them are of most interest today, namely grey, blue and green.

Currently, most of the hydrogen comes from natural gas (referred to as grey), but the process also produces a large amount of carbon waste. Most compounds in natural gas contain large amounts of hydrocarbons - hydrogen chemically bonded to carbon. Catalysts can break these bonds, but the excess carbon then forms CO₂.

The formation of blue hydrogen is based on the same process as grey hydrogen, with the additional capture and storage of carbon dioxide. This eliminates the emissions produced by gray hydrogen and thus the negative environmental impact of hydrogen production. The higher cost of producing blue hydrogen relative to gray hydrogen is associated with the installation of carbon capture, which is not present in the case of grey hydrogen [23].

An alternative promoted by major countries is to be blue hydrogen, whose production also relies on gas. However, according to studies conducted at Cornell University and Stanford, the carbon footprint of blue hydrogen, which is derived from natural gas, is up to 60% higher compared to burning diesel fuel. Consequently, the carbon footprint of its production compared to gray hydrogen is only 9÷12% lower. The researchers add that when the unabsorbed carbon dioxide is taken into account, as well as the large emissions of unburned methane associated with the use of natural gas during the production of blue hydrogen, the carbon footprint of its production is more than 20% higher than that of burning natural gas or coal [24].

The recommended hydrogen production is green hydrogen production, where only water and energy are needed, but not energy obtained from fossil fuels, but from renewable sources (RES). No carbon dioxide is produced at any stage during green hydrogen production – so it is zero-emission production. Obtaining hydrogen has disadvantages related to low efficiency of 30% resulting in high electricity requirements of 50 kWh/kg of hydrogen. Processes that use RES to produce hydrogen account for a negligible percentage of the global production of this gas, but provide an alternative to processes that use fossil fuels for this purpose. One of the rapidly developing forms of hydrogen production is the process of water electrolysis [23].

### *Hydrogen extraction from electrolysis*

Water electrolysis plays a key role in hydrogen generation based on the use of RES. Electricity supplied to electrolyzers is used to break water into two components - oxygen and hydrogen.

Equations 1 and 2 show the course of reactions on the anode (positive electrode) and cathode (negative electrode) of an alkaline electrolyzer, respectively. Equations 3 and 4 show the reactions occurring on the anode and cathode, respectively, of a proton exchange membrane electrolyzer [15]: 2*OH<sup>−</sup>*<sup>→</sup> 1 *O*<sup>2</sup> *+ H*2*O +* 2*e<sup>−</sup>* (1)

$$
2OH \rightarrow \frac{1}{2}O_2 + H_2O + 2e^-
$$
 (1) impact of SMR facilities.

$$
2H_2O + 2e^- \rightarrow H_2 + 2OH^-
$$
 (2) Partial oxidation of hydrocarbons

$$
H_2O \to 2H^+ + 2e^- + \frac{1}{2}O_2
$$
 The process  
directions is

$$
2H^+ + 2e^- \rightarrow H_2 \tag{4} \text{gen in process}
$$

*H*<sub> $\alpha$ **<sup>***H***</sup> <b>***H electrolysis* process *h*<sup>2</sup> *H*<sub>2</sub> (*H*<sub>2</sub> *M*<sub>2</sub> (*H*<sub>2</sub> *M*<sub>2</sub> (*H*<sub>2</sub> (*H*</sub> of water is presented by the Equation 5:

$$
H_2O \to H_2 + \frac{1}{2}O_2 \tag{5}
$$

very high purity, and the process is uncomplicaterators using water electrolysis are still expenrelation to the market demand for hydrogen proonly justified if the process is powered solely by Hydrogen produced by electrolysis has a ed and easy to operate. However, hydrogen gensive devices with relatively low power output in duction. Hydrogen production by electrolysis is renewable energy sources.

### *CnHm +* <sup>1</sup> 2 *nO*2<sup>→</sup> *nCO +* <sup>1</sup> 2 *Hydrogen extraction from hydrocarbon fuels mH*<sup>2</sup> (10)

Hydrogen extraction processes from hydro-Hydrogen extraction processes from hydro-<br>carbon fuels are based on the use of fossil fuels *C + H*2*O* <sup>→</sup> *CO + H*<sup>2</sup> (12) they are the main source of hydrogen supply for 1 *ndustry.* There are three main hydrogen extraction technologies for processes using hydrocarbon carbons (POX) and autothermal reforming (ATR). such as natural gas, oil and coal. At the moment, *OH*<sup>*D*</sup> are the main source of hydrogen supply for industry. There are three main hydrogen extrac*fuels:* steam reforming, partial oxidation of hydro-*H*2*O* <sup>→</sup> 2*H+ +* 2*e<sup>−</sup>+* <sup>1</sup>

#### $reforming$ *Steam reforming*

steam reforming of hydrocarbons. The reactions occurring during this process are described by the Equations 6 i 7 [15]: About 50% of the hydrogen is obtained by

$$
C_nH_m + nH_2O \to nCO + (n + \frac{1}{2}m) H_2
$$
 (6)

$$
CO + H_2O \rightarrow CO_2 + H_2 \tag{7}
$$

ost commonly used fuer<br>process is methane. The r process (8) and (9) are of the form:  $\sigma$  ,  $\theta$ reforming process is methane. The reaction equa-The most commonly used fuel in the steam tions for the steam methane reforming (SMR)

$$
CH_4 + H_2O \rightarrow CO + 3H_2 \tag{8}
$$

$$
CO + H_2O \rightarrow CO_2 + H_2 \tag{9}
$$

*Hocessing hydrocaroons under such conditions produces significant amounts of pollutants house* gases such as carbon dioxide. It is pos-<br>
∴H2 (12) sible to sequester carbon dioxide through carsignificantly reduces the adverse environmental bon capture and storage (CCS) facilities, which<br>capture and storage the education continuum with *O*<sub>2</sub> Processing hydrocarbons under such condiemitted into the atmosphere, including green-

drocarbons is another method to produce hydro-The process of partial oxidation of POX hydrocarbons is another method to produce hydrogen in processes using conventional fuels. The

reactions occurring during catalytic reforming are described by Equation 10, and for non-catalytic allows it to po *n n n n Equation* 11 [15]: *Couring during each yet reforming are* cheering to p

$$
C_nH_m + \frac{1}{2}nO_2 \rightarrow nCO + \frac{1}{2}mH_2 \tag{10}
$$

$$
C_nH_m + nH_2O \rightarrow nCO + (n + \frac{1}{2}m)H_2 \quad (11)
$$

*C F* the conversion of carbon monoxide  $\frac{1}{2}$  ing. At the mo *n*  $\alpha$  *no element* c *inserted into the equations of reactions occurring H*<sup>2</sup> *H*<sub>2</sub>**<sup>***OH</sup><sub>2</sub><sup>2</sup> <i>A***<sub>2</sub><sup>***OH***<sub>2</sub></sub>** *A***<sub>2</sub><sup>***OH***<sub>2</sub></sup>** *A***<sub>2</sub><sup>***OH***<sub>2</sub></sup>** *A***<sub>2</sub><sup>***OH***<sub>2</sub></sup>** *A***<sub>2</sub><sup>***D***</sup>** *A***<sub>2</sub><sup>***D***</sup>** *A***<sub>2</sub><sup>***D***</sup>** *A***<sup>2</sup>** *A***<sub>2</sub><sup>***D***</sup>** *A***<sup>2</sup>** </sup></sup> *CONDERE 12 MEXA CHAPP in close proximate in close proximate in the production of hydrogen, is obtained.*  $\frac{1}{2}$  or access to hydrogen.  $\frac{1}{2}$  **EV** and other<br>sponsible for the conversion of carbon monoxide  $\frac{1}{2}$  in  $\frac{1}{2}$  the mo  $\frac{1}{2}$   $\frac{1}{2}$  *H*<sub>2</sub> *H*<sub>2</sub> *M***<sub>2</sub> <b>***M*<sub>2</sub> *M*<sub>2</sub> *M*<sub>2</sub> *M*<sub>2</sub> *M*<sub>2</sub> *M*<sub>2</sub> *M*<sub>2</sub> *M*<sub>2</sub> *M*<sub>*M***</del><sub>2</sub> <b>***M*<sub>*M***</del><sub>2</sub> <b>***M*<sub>*M***</del><sub><b>***M***</del><sub>2</sub> <b>***M*<sub>*M***</del>**</sub></sub></sub></sub></sub> <sup>=</sup> + = + + , (15) ification process, which also plays a significant 2 2*OH<sup>−</sup>*<sup>→</sup> 2 *O*<sup>2</sup> *+ H*2*O +* 2*e<sup>−</sup>* (1) This reaction is shown by the relation (12): The reactions taking place in the reactor re*t*o CO<sub>2</sub> follow a course analogous to that of the  $\frac{1}{2}$  **CO**<sub>2</sub> (8)

$$
C + H_2O \rightarrow CO + H_2 \quad (12)
$$

# al conversio.<br>... *Autothermal conversion*

*E n c m conversion*<br>For this process, steam and air are fed into the ss, and the reactions characterizing BULK CARRI  $nH_2O + \frac{1}{4}nO_2 \rightarrow nCO + (\frac{1}{2}n)$ reforming process, seem and an arc red model **PNOPOLSIO**<br>reforming process, and the reactions characterizing **BULK CARRI**  $C_nH_m + \frac{1}{2}nH_2O + \frac{1}{4}nO_2 \rightarrow nCO + (\frac{1}{2}n)$ the ATR process are shown by Equation 13 [15]:  $H_2O + \frac{1}{4}nO_2 \rightarrow nCO + (\frac{1}{2}n + \frac{1}{2}m)H_2(13)$  $\frac{1}{2}$   $\frac{n+1}{2}$   $\frac{n}{2}$   $\frac{n+2}{2}$   $\frac{n+1}{2}$ 

<sup>1</sup> Inc essence of the energy conversion process a Panamax-ty<br>in fuel cells is the direct conversion of the chemi-<br>designed to ca *Cal energy of the fuel (hydrogen) into electrical* neoretical efficiency value<br>s is 83% [15], while the read In by the Equation  $14.$ The essence of the energy conversion process energy. The theoretical efficiency value for typienergy. The theoretical efficiency value for typical fuel cells is  $83\%$  [15], while the reaction oc- $\frac{1}{2}$  and  $\frac{1}{2}$  and  $\frac{1}{2}$  and  $\frac{1}{2}$  and  $\frac{1}{2}$  and  $\frac{1}{2}$  are  $\frac{1}{2}$  and  $\frac{1}{2}$  a during during energy conversion in these devices *n* these devices

$$
H_2 + \frac{1}{2}O_2 \rightarrow H_2O \tag{14}
$$

## $\overline{a}$ and land applications **Hydrogen fuel cells in marine<br>and land applications**

Fuel cells are seen as one of the most promising solutions for reducing harmful pollution. Already, the technology can power ships sailing short distances, as well as provide an auxiliary energy source on larger vessels. ABB and Hymegawatt fuel cell systems capable of powering<br>megawatt fuel cell systems capable of powering drogène de France (HDF) plan to jointly produce  $\alpha$  ocean-going ships [25].

The first example is the hydrogen plant togethship designed by Wärtsilä. The fuel cell system can operate in parallel with conventional propulsion  $\frac{1}{\sqrt{2\pi}}$ and relieve the energy burden on generators. Durreplace the operation of auxiliary engines [26]. An-<br>other application is the use of fuel cells to produce er with the LNG-fueled plant on the Viking Lady<br>chin decisened by Wörtsilä. The fuel call system can  $\alpha$  other application is the use of fuel cells to produce ing periods of low energy demand, this system can

electricity to power a shunting locomotive This allows it to perform its operating tasks close to a hydrogen refueling station. The locomotive is  $mH_2$  (10) equipped with a fuel cell module, hydrogen tanks and energy batteries [27]. <sup>m</sup> m<sub>p</sub><sup>m</sup>=

 $\frac{1}{2}$  *m)*  $H_2$  (11) Applications of the hydrogen system show the direction in which the entire maritime industry and other non-maritime industries are heading. At the moment, the hydrogen installation is not sufficiently developed to fully base ship proextructuring pulsion on it, but in the near future seagoing ships procurring a should be now and by hydrogen. For the moment should be powered by hydrogen. For the moment, only tugboats in ports and shunting locomotives are pioneering examples, which are used to work in close proximity to hydrogen refueling stations or access to hydrogen bottle swaps [28, 29]. <sup>not sumciently</sup><br><sup>1</sup> *m*ulsion on it.

# **CONVERSION OF CONVENTIONAL PROPULSION TO HYDROGEN PROPULSION OF A PANAMAX BULK CARRIER**

The ship selected for conversion was the bulk carrier of Polish Shipping "Giewont". It is rsion process a Panamax-type bulk carrier, which is mainly designed to carry dry-type bulk cargoes or semibulk cargoes by means of transmission belts, pumps, etc. It also transports coal, soybeans, rye, timber, etc. The basic parameters of the ship are shown in Table 1, while a graphic depicting the ship is shown in Figure 1.

# *Duration of the cruise*

The ship's route as adopted is entirely within the ECA control zone, according to the initial assumptions. The ship on the route Gdansk – Oslo has 540 nautical miles to travel. The ship's full voyage is shown in Figure 2.

Table 1. Basic information of the ship m/v Giewont [30]

Vessel name	m/v Giewont	
Number IMO	9452593	
<b>Dimensions</b>	$229\times32$ m	
Carrying capacity	79649 tons	
Gross tonnage	43506 tons	
Vessel type	<b>Bulk Carrier</b>	
Engine speed	127 rev/min	
Main engine power	11 060 kW	
Construction year	2010	



**Figure 1.** Photo of the ship m/v Giewont [30]



**Figure 2.** The assumed route of the ship [31]

Equation 15 shows the total duration of the ship's<br>2020 according to gradetermined quidelines [22] voyage according to predetermined guidelines [32]: <sup>2</sup> *m) H*<sup>2</sup> (11)

$$
\tau_{\rm c} = \tau_{\rm jm} + \tau_{\rm p} = \tau_{\rm j} + \tau_{\rm m} + \tau_{\rm p} \tag{15}
$$

where:  $\tau_c$  – total cruise duration [h],  $\tau_{im}$  – ship's stay at sea [h],  $\tau_j$  – ship sailing time [h],  $\tau_{\rm p}$  ship's stay in ports [h],  $\tau_{\rm m}$  – duration *of maneuvers at sea [h]. CnHm +* <sup>1</sup>

Knowing the vessel's sailing range, i.e. 540 2 Mm, the vessel's sailing time can be calculated from the formula 16:

$$
\tau_j = \frac{R}{v_{ex} - \Delta_v} \tag{16}
$$

 $\frac{1}{2}$   $\frac{1}{2}$   $\frac{1}{2}$   $\frac{1}{2}$   $\frac{1}{2}$   $\frac{1}{2}$   $\frac{1}{2}$   $\frac{1}{2}$  average speed drop effect of hull entrainment, etc. (for a laden where:  $\tau_j$  ship sailing time [h],  $R$  – sailing range [Mm],  $v_{ex}$  – operational speed of the ship due to worse weather conditions, negative voyage it was assumed  $\Delta_{\nu} = 1$ kt).

By substituting data into the formula 16:

$$
\tau_j = \frac{540 \, Mm}{12 \, kt - 1 \, kt} = 42 \, h.
$$

Thus, the sailing time  $\tau_j$  is 42 hours.

ration of maneuvers during the entire trip: Using Equation 17, we can determine the du-

$$
\tau_{\rm m} = a_{\rm m} \cdot \tau_{\rm j} \tag{17}
$$

where:  $\tau_{\text{m}}$  – duration of maneuvers at sea [h],  $a_m$ – maneuvering time factor, depending<br> **a** – maneuvering time factor, depending<br> **burgely** on the number of ports and other assumed  $a_m = 0.15$ ),  $\tau_j$  –  $(46)$ largely on the number of ports and other ship sailing time [h].

sinp sating time [n].<br>Substituting the data into the formula, we get (17):

$$
\tau_{\rm m} = 0.15 \cdot 42 \text{ h} = 6 \text{ h}
$$

Thus, the duration of the maneuvers is 6 hours.

**Another component of time in a ship's voy**age is the time spent in the vessel's port, we can

.

 $\alpha$ <sup>18</sup> calculate this from Equation 18. Of course, this *Correlation varies with the type of vessel, the mo-*<br> *Nominal consumption of light fuel* dernity of unloading and loading facilities and ma  $\frac{1}{2}$  many other variables: 2*H*2*O + 2e<sup>−</sup>*<sup>→</sup> *H*<sup>2</sup> *+* 2*OH<sup>−</sup>* (2) 2*OH<sup>−</sup>*<sup>→</sup>

$$
\tau_p = \left(1 - \alpha_{jm}\right) \cdot \tau_c = \frac{1 - \alpha_{jm}}{\alpha_{jm}} \cdot \tau_{jm} \qquad (18) \qquad \text{w}
$$

where:  $\tau_{p}$  ship's stay in ports [h],  $a_{jm}$  – coeffi-<br>by the main engine cient of the time a vessel stays at sea (for cruise duration [h],  $\tau_{jm} - \tau_j + \tau_m$  [h]. bulk carriers assumed  $a_{\text{in}} = 0.8$ ),  $\tau_c$  total there:  $\tau_{p}$  ship's stay in ports [h],  $a_{im}$  – coeffi- $\tau_{\text{jm}}^2 = 0.0$ ,  $\tau_{\text{c}}^2$ <br>cruise duration [h],  $\tau_{\text{jm}} - \tau_{\text{j}} + \tau_{\text{m}}$  [h]. 2*H+ +* 2*e<sup>−</sup>*<sup>→</sup> *H*<sup>2</sup> (4)

By substituting the data into Equation 4, it  $\frac{1}{4}$   $\frac{1}{1}$   $\frac{1}{1}$  was obtained: *C + H*2*O* <sup>→</sup> *CO + H*<sup>2</sup> (12) *CO + H*2*O* <sup>→</sup> *CO*<sup>2</sup> *+ H*<sup>2</sup> (7) *CH<sub>4</sub> H<sub>2</sub> C*<sub>4</sub> *C*<sub>4</sub> *C* + *n*<sub>2</sub><sup>*O*</sup> *n*<sub>2</sub><sup>*O*</sup> *n*<sub>2</sub><sup>*O*</sup> *n*<sub>2</sub><sup>*O*</sup> *n*<sub>2</sub><sup>*O*</sup> *n*<sub>2</sub><sup>*O*</sup> *n*<sub>2</sub><sup>*O*</sup> *CO + H*2*O* <sup>→</sup> *CO*<sup>2</sup> *+ H*<sup>2</sup> (7) *H*<sub>2</sub> substituting the dat *A*<sub>2</sub> *H*<sub>2</sub> (3) *H*<sub>2</sub>

$$
\tau_p = \frac{1 - 0.8}{0.8} \cdot 48 \, h = 12 \, h
$$

 $\frac{60}{2}$  otal time in no <sup>=</sup> + = 48 ℎ + 12 ℎ = 60 ℎ. The ship's total time in port is 12 hours. *n*e ship's total time in port is 12 hours. *C SHP S iOtal HHC III pOL iS ch*<sup> $\alpha$ </sup><sup></sup> *c*<sub>2</sub> *kotal time in port is 12 hours. CO + H*2*O* <sup>→</sup> *CO*<sup>2</sup> *+ H*<sup>2</sup> (9) <sup>2</sup> *m) H*<sup>2</sup> (6)

Adding up all the components calculated earget the total duration of the voyage: lier and substituting them into Equation 15, we set the total dynamics of the systems. *n*<sub>2</sub>→ *n*<sub>2</sub>  $\frac{1}{2}$  and substituting them mo Equation 1.<br>
get the total duration of the voyage: **CO**<sub>2</sub> + H<sub>2</sub>O **+** H<sub>2</sub> (7) + H<sub>2</sub> *COMPONERS CALCURAC* 

$$
\tau_c = \tau_{\text{jm}} + \tau_p = 48 h + 12 h = 60 h
$$

Thus, the total duration of the cruise is 60 hours. */*  $\frac{1}{2}$   $\frac{1}{2}$ *O*2<sup>→</sup> *H*2*O* (14) *c* <sup>*n*</sup> <sup>*n*</sup> <sup>*p*</sup><br>*he* total duration of the cruise is 60 hours.

Due to the fact that the ship is designed for *be taken into account that there will be possible into account that there will be possible* breaks are not necessary.  $\mu$  but to the fact that the sinp is designed for  $\mu$ <br>hydrogen propulsion during the voyage, it should  $\frac{1}{\pi}$  inter refueling, but on the chosen route such *E* and *necessary*. The *nosen* route such *years*, for this chosen *second* the chosen route such *secondary*. *H*<sub>2</sub> *Due* to the fact that the ship is designed for lrogen propulsion during the voyage, it should *n*<sub>2</sub> to the fact that the ship is designed for *CnHm +* <sup>1</sup> <sup>=</sup> + = + + , (15) *C*  $\frac{1}{2}$  *C* + *C* + *H*<sup>2</sup> (12) (12) (12) *H*<sup>2</sup> *+* <sup>1</sup>

#### *Actual specific fuel consumption*  (16) *and CO<sub>2</sub>* emissions  $11 - 42 - 6212$  $\overline{z}$  $\overline{a}$

The fuel with a sulphur content of  $0.1\%$  and a sinked and amounts to soc The fuer with a supplier content of 0.1% and a<br>density of  $\rho = 863.4 \text{ kg/m}^3$ , which is used in the ECA  $\alpha$  zones, was accepted for the calculations. The value<br>  $\alpha$  f the gracific fiel computation of the MAN D  $\beta$ W zones, was accepted for the calculations. The value<br>of the specific fuel consumption of the MAN B&W<br> $7860 MeB$ or the specific fuel consumption of the MAN B&W<br>
7S50MC-C engine, which results from the technical<br>
or  $\frac{175 \times 0 \text{N}}{4 \text{N}}$  $\alpha$ ,  $\beta$ ,  $\beta$ ,  $\beta$ ,  $\beta$ ,  $\beta$ ,  $\alpha$ ,  $\beta$ ,  $\beta$ ,  $\beta$ ,  $\beta$ ,  $\beta$ ,  $\gamma$ ,  $\beta$ ,  $\gamma$ ,  $\beta$ ,  $\gamma$ ,  $\beta$ ,  $\gamma$ ,  $\alpha$ ,  $\alpha$ ,  $\beta$ ,  $\gamma$ ,  $\alpha$ ,  $\gamma$ , and operational documentation, is  $g_e = 1/5$  g/kWh.<br>The actual specific diesel consumption was calculated from the formula  $[32]$ :<br> $w_i^u$ 

$$
g_e^{on} = \beta \cdot g_e \frac{w_d^u}{w_a^{on}} [g/\text{kWh}] \qquad (19) \qquad \text{erage bu} \\ \text{CO}_2, \text{ass}
$$

where  $\beta$  – coefficient of limiting fuel consumption  $\frac{W[11, 11]}{S}$ <br>above the normative value, given and guar-<br> $\frac{1}{2}$ was assumed,  $g_e$  [g/kWh] – specific, nomi-<br>nal consumption of contractual fuel given by  $\frac{1}{221}$ , the manufacturer of the engine,  $w_d^u$  [kJ/kg]  $=$   $\frac{1}{221}$ . − calorific value of contractual fuel given by<br>the manufacturer of the engine,  $w_d^u = 42700$ where  $\beta$  – coefficient of limiting fuel consumption will increase by  $\beta$ anteed by the engine manufacturer,  $\beta = 1.03$ <br>was assumed,  $g \left[ g / kWh \right]$  – specific, nomiwas assumed,  $g_e$  [g/KWn] – specific, nominal consumption of contractual fuel given by<br>the manufacturer of the angine  $\mathbb{R}^d$ . [[*FIIco] e* galeric, *e*<br>contractual fu  $\frac{d}{dx}$  – calorific value of contractual fuel given by  $\frac{d}{dx}$  –  $\frac{d}{dx}$  +  $\frac{d}{dx}$  $=$   $\frac{1}{2}$  assumed calorific value  $kJ/kg$ ,  $w_q^n$  [ $kJ/kg$ ] – assumed calorific value where  $\rho$  – coefficient of finding fuel  $\alpha$ ,  $\rho$  $w_d^{on}$  [kJ/kg] – assumed calorific value of diesel oil, where  $\beta$  – coefficient of limiting fuel consumption will increase by \$1.4 mi  $\lim_{d \to \infty} \frac{d}{dx}$  [Ke/*K*<sub>2</sub>] (assumed curricle value) anced by the eighte manufacturer,  $p = 1.03$  and  $\sigma g_2$  recession, assuming the time assumed  $q_1$  [or bulk carriers] change significantly:

$$
g_e^{on} = 180.67 \text{ g/kWh}.
$$

#### *Fuel consumption during the cruise =* 180.67 *g*/*kWh. = β∙ ge∙*  $g$  the cruise *e a leonsumption during the cri*mination <sup>=</sup> + = 48 ℎ + 12 ℎ = 60 ℎ. s Fuel consumption during the cruis  $\cdots$  and  $\ddot{\phantom{a}}$  $\frac{1}{\sqrt{h}}$  stays in ports  $\frac{1}{\sqrt{h}}$ , construction develops the surface course, this the consumption during the cruise.<br>all the mo ion 18. Of course, this Fuel consumption during the cruise

*= β∙ ge∙*

Nominal consumption of light fuel by the main engine  $(G_g^{on})$ :  $\overline{\phantom{a}}$ umption of light fu@<br>.. **E**<br>
Nominal consumption of light fuel by the  $G_g^{on} = g_e^{on} \cdot N_n^* \cdot 10^{-4}$  $N^* = 10^{-6}$  F  $/$ 

$$
G_g^{on} = g_e^{on} \cdot N_n^* \cdot 10^{-6} \, [\text{t/h}] \tag{20}
$$

[*g*/*kWh*] (19)

· , (18)

· , (18)

where:  $g_e^{on}$  – actual specific light fuel consumption *O*<sup>2</sup> (3)  $N_n^*$  – nominal power of the main engine  $(N_n^* = 11060 \text{ kW})$ . by the main engine  $(g_e^{on} = 180.67 \text{ g/kWh})$ ,  $(N_n^* = 11060 \text{ kW}).$  $e^{\text{pre}}$ :  $g_e^{on}$  – actual speci  $(N_n^* = 11060 \text{ kW}).$ 

 $\sum_{i=1}^{\infty}$  statistical  $\binom{n}{i}$ ,  $\binom{n}{j}$  and  $\binom{n}{j}$  at sea (for a version bulk carriers) at a version of the time and  $\binom{n}{j}$ *After inserting into the formula* After inserting into the formula 23 th<br>
and fuel consumption is respectively: *<sup>=</sup>*83.58 *.* After inserting into the formula 23 the nomi-

$$
G_g^{on} = 1.99 \text{ t/h}.
$$

*m<sub>g</sub>* + 1.99 *m*.<br>With information that this vessel will sail 42 the fuel consumption: **hours on the route Gdansk** – Oslo, you can count

$$
G_g^{on}=42\cdot 1.99\,\frac{t}{h}=83.58\,\frac{t}{route}
$$

route 2 times a week and the year consists of an average of 52 weeks, you can estimate the fuel consumption for a year: Due to the fact that the vessel operates this

$$
G_g^{on} = 83.58 \cdot (2 \cdot 52) = 8692.32 \frac{t}{year}
$$

1ble<br>
wears, the fuel consumption has been calculated<br>
<u>consulting</u> Suppose that the vessel will sail more for 10 for this period:

$$
G_g^{on} = 8692.32 \cdot 10 = 86923 \frac{t}{10 \, year}
$$

*Assuming the world price of low-surphured*<br>is fixed and amounts to \$600 per ton [33] it is possible to estimate the cost of fuel consumed for a.  $(10 \text{ years})$ : given period (10 years): Assuming the world price of low-sulphur fuel

$$
86923 \, t \cdot 600 \, \text{S} = 52153800 \, \text{S}.
$$

related to  $\mathcal{O}_{22}^{\circ}$  emissions, since sinplying is  $\mathcal{O}_{22}$  ered by the EU emissions trading system (ETS) lated from the formula [32]: as of January 1, 2024. Operating costs for an avas of January 1, 2024. Operating costs for an average bulk carrier emitting about 16000 tons of  $y_e$  =  $\beta$  s<sub>e</sub>  $w_a^{\text{on}}$  (g/k w ii)  $\text{CO}_2$ , assuming it trades only between EU ports, = 1798.7 + 11060 = 12858.7 . related to  $CO<sub>2</sub>$  emissions, since shipping is covwill increase by \$1.4 million annually, [34], i.e. \$14 million over 10 years. The total cost of fuel change significantly: To the cost of fuel, you have to add charges will increase by \$1.4 million annually, [34], i.e.<br>\$14 million over 10 years. The total cost of fuel and  $CO<sub>2</sub>$  fees is, assuming the price does not re significantly:<br>52153800 + 14000000 = 66153800 \$.

= 60 A · 242<br>- 60 A · 242 · 242 · 242 · 242 · 242 · 242 · 242 · 242 · 242 · 242 · 242 · 242 · 242 · 242 · 242 · 242 · 242 ·

# n of the current level of CO . emissions (carbon footprint)<br>*L* availably light discal 1 *Calculation of the current level of CO2*

 $\theta$  ∗ the  $\theta$  *=* 180.67 *g*/*kWh.* Low-sulphur light diesel, that is used to propel the ship, has density of  $\rho = 863.4 \text{ kg/m}^3$ , therefore:

$$
0.863 kg fuel = 1 dm3 fuel
$$

 $G_g^{on} = 86923t = 86923000$  kg,  $G_g^{on}$  = 100721900 dm<sup>3</sup>.

 $\alpha$  the current level of  $CO_2$  emissions According to [35] T and or dieser produces 2.0<br>kg of  $CO_2$ , so the current level of  $CO_2$  emissions is: According to [35] 1 dm<sup>3</sup> of diesel produces 2.68

> *<sup>=</sup>*42 ∙ 1.99 <sup>ℎ</sup> *<sup>=</sup>*83.58 *. CO2 emissions* = 100721900 ∙ 2.68 *= =*261745662.56 kg = 261745.66 t.

# **Main engine and its replacement with alternative electric motors**

Variables characterized by a certain range of values were selected to be as close as possible to the tool values MAN & Turbo recommends. The computerized engine application system (CEAS) performs all the necessary calculations, as well as the dimensioning for the main drive, interacting with the installations based on the basic data entered [36]. Based on system-generated calculations and data, the designed fuel cell plant will be converted from the systems, parameters and equipment generated by CEAS for conventional propulsion. The design assumptions are presented in Table 2.

Already knowing the power of the conventional main engine selected by CEAS, alternative electric motors can be selected to serve as the ship's main propulsion system. The MAN B&W 7S50MC-C main engine generates 11060 kW and has a speed of 127 rpm. Standard electric motors produced in series reach power outputs of up to a few kW, depending on the manufacturer. In this case, to meet the needs of the ship's engine room and the ship as a whole, it is necessary to select motors that will match the power output of the conventional main engine. Accordingly, based on the calculations of the CEAS program, 2 high-voltage electric motors VYBO 5500 kW H27R shown in Figure 3. were selected, while its basic parameters are shown in Table 3 [37].

**Table 2.** Design assumptions [36]

Engine model	MAN B&W 7S50MC-C	
Type of engine supercharging	Conventional (turbocharger)	
Load adjustment	High load	
Thruster type	4-wing fixed pitch screw	
Cooling water system	Central cooling system	
Cooling water temperature	25 °C (condition ISO)	
Normal working conditions	100%	



**Figure 3.** View of the high-voltage electric motor VYBO 5500 kW H27R [37]

**Table 3.** Basic parameters of the VYBO 5500 kW H27R engine [37]

Engine name and model	<b>VYBO 3700 kW H27R</b>	
l Power	5500 kW	
Nominal voltage	3 kV	
Frequency	60 Hz	
Rotational speed	2900 rev/min	

### **Reduction gear on the main drive train**

Getting rid of the MAN B&W 7S50MC-C diesel main engine and inserting two VYBO 5500 kW H27R electric motors in its place, the reduction gearbox in the ship's main propulsion system must be modified. In order not to generate additional costs, the main drive system remains unchanged with the only modification being the replacement of the reduction gearbox. The reduction gear must be selected so that the drive system can be driven by two electric motors that operate at 2900 rpm, while the thrust shaft can remain at the optimal speed it was designed for, which is 100–127 rpm. A multi-stage reduction gearbox will ensure the optimum speed of the drive train shaft.

## **Power requirements for converting conventional motors to electric motors**

The auxiliary engines that were on the ship should be replaced with electric motors powered by fuel cell energy. These engines are deliberately selected independently of the main engines in order to be able to operate independently during operation. In place of conventional motors, 3 electric motors will be installed, so that, as in the previous application, as many motors can be loaded as electric power is required. Knowing the power of the motor, it is easy to calculate from relation (24) the power of electricity (formula proposed by Michalski) [32]:

$$
N_{\rm el} = 0.08912 \cdot N_{\rm n} + 812.7\tag{21}
$$

where:  $N_{el}$ – estimated power of the ship's power plant [kW],  $N_{\rm n}$  – nominal power of the selected main motor [kW], 0.08912 – directional coefficient of the trend line, 812.7– coefficient resulting from the intersection with the axis of ordinates of the trend line [kN].

Thus, substituting the data from Table 1 into the formula, we get the result:

> $_{\rm{el}}$  = 0.08912 · 11060 kW + +812.7 kW = 1798.7 kW

### **Fuel cell module**

The fuel cell module is intended to replace the main and auxiliary engines on a Panamax marine vessel. In order to select the appropriate module, as well as their quantity, it is necessary to add up the total power produced by one MAN B&W 7S50MC-C main engine and three Wärtsilä 645W4L20 auxiliary engines. For this purpose, the relationship (25) was used:

$$
N = Nel + Nn
$$
 (22)

where:  $N_{el}$  – estimated power of the ship's power plant [kW],  $N_n$  – nominal power of the selected main motor [kW], *N* – the sum of the power of the main engine and the ship's power plant [kW].

Substituting the data from relation (22) and the power of the MAN B&W 7S50MC-C main engine, we get the following result:

*N* = 1798.7 kW + 11060 kW = 12858.7 kW

Thus, the estimated power of the main engine and the ship's power plant is 12858.7 kW, for further consideration, the power was taken as 13000 kW.

Knowing a ship's power requirements makes it easy to select the fuel cell modules needed to convert conventional propulsion to hydrogen propulsion. Ballard offers Ballard's FC wave fuel modules, which are adapted for use in the marine industry.

One Ballard's 1000 kW FC wave fuel cell module generates a power rating of 1000 kW, so 13 such modules will be required to meet the ship's needs, for a total of 13,000 kW. These modules can be installed in place of the main engine, as the dimension of one such module is 1209×741×2195 mm. An additional advantage of using fuel cells is that more fuel cell modules can easily be added if the ship needs more power. Ballard's modules are cooled by liquid, more precisely by a mixture of water and glycol in a 50/50 ratio. For this purpose, the existing cooling system of the main engine can be successfully used. Thus, if the aver-<br> $\frac{1}{2}$ engine can be successfully used. Thus, if the aver-<br>age hydrogen consumption for a 1000 kW module is  $16 \div 18.6$  kg/h [38], sofrom the simple rela-86928 **to ∗ 18.0 kg/n** [58], solitom the simple relationship (26), you can calculate the hydrogen consumption for all modules [38]: 639 600 500 **600** ± 6615 600 ± 6615 600 ± 6615 600 ± 6615 600 ± 6 ydrogen consumption for a 1000 kW<br> $\div$  18.6 kg/b [38], sofrom the simp

$$
G_{\rm w m} = 13 \cdot G_{\rm jm} \tag{23}
$$

where:  $G_{wm}$  average hydrogen consumption of  $\frac{G_{wm}}{m}$  are average *if* are generally consumption of hydrogen consumption of one fuel cell  $\text{module } [\text{kg/h}]$ .

So, substituting the data into equation  $(26)$ , we get the result:

$$
G_{wm} = 13 \cdot 16 \frac{kg}{h} = 208 \frac{kg}{h}
$$

and

$$
G_{wm} = 13 \cdot 18,6 \frac{kg}{h} = 241,8 \frac{kg}{h}
$$

 $\frac{1}{2}$ rated power by an ship modules is  $208 \div 241$ <br>which is approximately  $208 \div 242$  kg/h. The average hourly hydrogen consumption at  $d$  nexus by all ship modules is  $208 \div 241.8$  kg/h rated power by all ship modules is  $208 \div 241.8$  kg/h,

# torage tanks <sup>=</sup> , (25) **Hydrogen storage tanks**

ng to the introduction in th<br>it hydrogen is a problemat  $\alpha$ conventional propulsion to hydrogen propulsion,<br>**Legendaria** (HEO) and projected the Li Q4DO) fuel tanks will prove unnecessary. They will be able<br>the same are additional bellett taken as in the fattern the tanks will prove unnecessary. They will be able<br>to serve as additional ballast tanks, or in the future tem converted to hydrogen storage tanks. Referring to the introduction in the article, it can be noted that hydrogen is a problematic medium for<br>transportation as well as storage. In order to convert be noted that hydrogen is a problematic medium for<br>transportation as well as storage. In order to convert heavy fuel oil (HFO) and marine diesel oil (MDO) with the development of the hydrogen storage sys-

be adapted to store hydrogen storage. The hold for diapped to store hydrogen storage. The hotel is an ideal location, as the hydrogen tanks, acpur-<br>also away from the entire hydrogen cell installation. but the company of the storage tax standard single ping containers with hydrogen storage tanks in<br>its offer. The composite hydrogen storage cylin-As assured by the manufacturer, such a solution **15100.8 ° 2000 ≥ 2000** and 2000 **D** and 2000 **D** and 2000 **D** and 2000 **m** between the ship, the first cargo hold will have to for all raceal foculton, as the hydrogen tensis, according to the PRS regulation, should be located zh away from the entire hydrogen cen instantation.<br>
<u>Execute</u> 2. Dutch company H2 storage has standard shipder is manufactured from resin and carbon fiber.  $\overline{2}$ 

provides greater storage capacity relative to steel and aluminium tanks.

A shipping container with standard dimensions of 1200cm×260cm×239cm will be equipped with 100 such cylinders. The entire container will be capable of storing 1400 kg of hydrogen stored at 700 bar. The containers can be connected in series through the manufacturer's specially adapted installation, providing a large fuel buffer on board. The only limitation is the payload capacity of the containers on the ship. A cross-section of the entire container is shown in Figure 4.5201 the entire container is shown in Figure 4 [39].

Already knowing the possibility of storing process. hydrogen in shipping containers, one can proceed with calculations. One container can store 1400 kg of hydrogen. Based on the results from the previous calculations according to formulas (21) and (26), it is possible to calculate the hydrogen demand for the entire duration of the voyage from relation (27). The upper limit of the average hourly hydrogen burn will be used for the calculation to ensure an adequate safety buffer.

$$
G_{\rm cr} = \tau_{\rm c} \cdot G_{\rm wm} \tag{24}
$$

where:  $G_{cr}$  – average hydrogen consumption during the entire voyage [kg],  $\tau_c$  – total cruise duration [h],  $G_{wm}$  – average hydrogen conduration [h],  $G_{\rm{wm}}$  – average hydrogen cor<br>sumption of all fuel cell modules [kg/h].

The upper limit of the average hourly hydro-Fire upper mint of the average hourly hydrogen combustion will be used in the calculations to provide an adequate safety buffer. By substituting provide an adequate safety buffer. By substituting the previously calculated data into Equation 27, we get the following: and  $\overline{a}$ 

$$
G_{cr} = 60 h \cdot 242 \frac{kg}{h} = 14520 kg
$$

I hus, the average hydrogen consumption<br>during the entire cruise is 14 520 kg.Then, from a Thus, the average hydrogen consumption<br>and the article equips is  $14.520$  kg. Then, from a simple calculation (28), the number of hydrogen simple calculation (28), the number of hydrogen<br>containers to be placed in the hold for the dura-<br>tion of the vertex and he calculated: tion of the voyage can be calculated: a calculation (28), the number of l  $\frac{64}{5}$   $\frac{64}{5}$   $\frac{1}{1}$   $\frac{1}{1}$   $\frac{1}{1}$   $\frac{1}{1}$ ble calculation (28), the number of hy<br>ainers to be placed in the hold for the

$$
L_k = \frac{G_{cr}}{W_{wk}}\tag{25}
$$

 $\frac{1}{k}$  hydrogen consumption during the entire  $\frac{1}{k}$ . weight of bydrogen in  $\frac{1}{2}$  voyage [kg],  $W_{wk}$  – weight of hydrogen in one container [kg] one container [kg]. . where:  $L_k$  – number of containers,  $G_{cr}$  – average  $L_k$  – number of containers,  $G_c$ , by *dregger* consumption during

get the result of the number of containers:  $\mathbf{S}$ : By substituting the data into Equation 28, we duing the data into Eq.

$$
L_k = \frac{14520 \text{ kg}}{1400 \text{ kg}} = 10.38
$$

The number of containers needed to meet the  $\int_C$  is invariance in the term of  $\int_C$  is approximately up to the he sin β s hydrogen needs is approximately up to the top figure gives 11 containers of hydrogen. The number of containers needed to meet the<br>ship's hydrogen needs is approximately up to the<br>top figure gives 11 containers of hydrogen.

may change during different routes of the ship.<br>The velue given wes calculated on the basis of the  $n_{\rm SN}$ -Osio route. *Gcourse*, the number of hydrogen containers of course, the number of hydrogen containers  $\alpha$  change during different routes of the shin Of course, the number of hydrogen containers<br>may change during different routes of the ship. The value given was calculated on the basis of the Gdansk-Oslo route. The value given was calculated<br>Gdansk-Oslo route.

## Hydroaen consumption and CO, emissions *Hydrogen consumption and CO<sub>2</sub> emissions*

Due to the fact that the ferry operates this<br>
route 2 times a week and the year consists of an<br>
give a success of 52 weeks you are estimate the hydro  $\frac{1}{2}$  gen consumption for a year:  $\mathbf{r}$ : Due to the fact that the ferry operates this average of 52 weeks, you can estimate the hydroa die year consistent

$$
G_{cr} = 14.52 \cdot (2 \cdot 52) = 1510.08 \frac{t}{year}.
$$

years, the hydrogen consumption has been calcu-<br>lated for this period: Suppose that the vessel will sail yet for 10 lated for this period: ssee Am

$$
G_{cr} = 1510.08 \cdot 10 = 15100.8 \frac{t}{year}.
$$

fixed and amounts to 2\$ per kg [40] it is possible<br>to estimate the cost of fuel consumed for a given to estimate the cost of fuel consumed for a given Assuming the world price of hydrogen is period (10 years):

m a  $15100.8 \cdot 2000 = 30201600$  \$.



**Figure 4.** Cross-section of a hydrogen storage shipping container from H2 storage [39]

The total  $CO_2$  emissions from hydrogen consist of production, storage and transportation.

The production of one ton of hydrogen generates about ten tons of  $CO<sub>2</sub>[41]$ , therefore:

 $[CO_2]$ <sub>production</sub> = 15100.8  $\cdot$  10 = 1 = 151008 t.

Currently, 76% of the hydrogen sourced is gray hydrogen sourced from fossil sources by which they contribute to high greenhouse gas emissions (including  $CO_2$ ). After hydrogen is produced, it has to be stored and transported to the end-users. Currently, two storage methods exist, physical hydrogen storage (high-pressure hydrogen storage, liquid hydrogen storage and cryo-compressed hydrogen storage) and chemical hydrogen storage.

On the ship, the hydrogen will be stored in tanks in gaseous form, for which, during storage and transport,  $CO_2$  emissions are, according to [42], about 500 kg of  $CO_2$  per ton of hydrogen per 100 km. The ship has a distance to travel of 540 Mm, or 1,000 km. This means that  $CO_2$  emissions along this route will be 5 t per ton of hydrogen and eventually:

$$
[CO2]storage + transport = 15100.8 \cdot 5 = 75504 t.
$$
  
\n
$$
[CO2]p+s+t = 151008 + 75504 = 226512 t.
$$

# **Inverter to convert direct current to alternating current**

An inverter is an electrical device that converts direct current into alternating current. Fuel cells produce direct current, but the entire electrical system on the ship and all the electric motors run on alternating current, so the hydrogen system needs the aforementioned inverter. The device will be selected for hybrid operation, i.e. with batteries and the ship's power grid. Knowing the power of the fuel cell modules from relation (10), we can calculate which inverter should be used on the ship [43]:

$$
0.7 \cdot P_{\text{MAX(MOD)}} < P_{\text{NOM(INV)}} < 1.2 \cdot P_{\text{MAX(MOD)}} \text{ (26)}
$$
\n
$$
\text{where: } P_{\text{NOM(INV)}} - \text{converter power [kW]}, P_{\text{MAX(MOD)}} - \text{power of fuel cell modules [kW]}.
$$

Knowing the total power of the fuel cell modules calculated relation 6, we get the condition 10:

$$
0.7 \cdot 1300 \text{ kW} < P_{NOM(INV)} \text{ kW} < 1.2 \cdot 1300 \text{ kW},
$$
\n
$$
9100 \text{ kW} < P_{NOM(INV)} \text{ kW} < 15600 \text{kW}.
$$

Based on these calculations, an inverter from INGECON SunPowerstation CON40 NA/NA/FA was selected. It is a power station with a maximum capacity of 4920 kVA, i.e. 3936 kW, equipped with a transformer and electrical switchgear. The most important aspect is the possibility of installing several such inverters in one installation. Figure 5 shows the selected inverter in the form of a shipping container. The ship will require three INGECON SunPowerstation CON40 NA/NA/FA inverters, which will operate in parallel [43].

### **Batteries in the hydrogen system**

Knowing the energy requirements of the ship, it is necessary to select the appropriate batteries and their capacity. The task of batteries in a ship's hydrogen system is mainly to secure the ship in electricity in the event of a total failure of the fuel cells. In addition, the batteries will compensate for temporary energy requirements.

The voltage that the fuel cells will generate is 650 VDC, so the 12-volt batteries will be connected in series, resulting in a summation of voltages while maintaining the original capacity. In order to extend the life of the batteries, their capacity should be doubled to avoid deep discharge. Connecting 54 batteries in series will result in a rounded 650 volts.



**Figure 5.** Station view INGECON SunPowerstation CON40 NA/NA/FA [43]

Formula 11 allows you to calculate the capacity of the batteries:

$$
C = \frac{2 \cdot (N \cdot \tau_c)}{U} \tag{27}
$$

of the power of the main engine and the of the power of the main engine and the ship's power plant [kW],  $\tau_c$  – total cruise where:  $C$  – battery capacity [kAh],  $N$  – the sum duration [h],  $U$  – system voltage [V].

When substituted into the formula, we get:

$$
C = \frac{2 \cdot (13000 \, kW \cdot 60 \, h)}{650 \, V} = 2400 \, kAh.
$$

 $\frac{1}{650}$   $\frac{1}{100}$   $\frac{1}{2400}$   $\frac{1}{100}$ . lithium-iron-phosphate battery from Fronius Solar Battery was selected. The battery is characterized by short charging time, possible deep discharge, which is important for battery life. Fronius assures that it can select the parameters of the battery for a specific project on special request. A block diagram of the hydrogen system created for a Panamax-type ship, using all the selected components, is shown in Figure 6.

# **ANALYSIS OF THE POSSIBILITY OF USING A HYDROGEN FUEL CELL TO PROPEL A PANAMAX BULK CARRIER**

### **Technical analysis**

The ship's route as adopted is entirely within the ECA control zone. The ship on the route Gdansk - Oslo has 540 nautical miles to cover. The total duration of the voyage with sailing time, with maneuvering and stopping in port is 60 hours. Due to the fact that the ship is designed for hydrogen propulsion during the voyage there may be possible inter refuelling, but on the chosen route such breaks are not necessary. Knowing the power of the conventional main engine, alternative electric motors were selected to serve as the ship's main propulsion system. The main engine generates 11060 kW of power, and its speed is 127 rpm. To meet the needs of the ship's engine room and the ship as a whole, 2 high-voltage electric motors were selected to match the power output of the conventional main engine. The auxiliary engines that were on board the ship are to be replaced with electric motors powered by fuel cell energy. These motors are deliberately selected independently of the main engines in order to be able to operate independently during operation.

In place of conventional motors, 3 electric motors will be installed so that, as in the previous application, as many motors can be loaded as electric power is needed.

The fuel cell module is designed to replace the main and auxiliary engines on a ship. In order to select the right module, as well as their number, it is necessary to add up the total power produced by one main engine and three auxiliary engines. To meet the needs of the ship, 13 such modules will be required, which will have a total power output of 13,000 kW. These modules can be installed in place of the main



**Figure 6.** Block diagram of hydrogen system on Panamax ship: 1 – hydrogen tanks, 2 – air blower, 3 – electric electric motors, 4 – hydrogen fuel cell module, 5 – water tank, 6 – DC to AC inverter, 7 – batteries, 8 – other energy consumers, 9 – electric main engines, 10 – gearbox, 11 – propeller shaft, 12 – propeller, hydrogen, air, water, electricity, shaft line

engine. Ballard's modules are cooled by liquid, more precisely by a 50/50 mixture of water and glycol, and the existing cooling system of the main engine can be successfully used for this purpose.

The ship will need to adopt the first hold for hydrogen storage space. The cargo hold is an ideal location because the hydrogen tanks, according to the PRS regulation, should be in a place away from the entire hydrogen cell installation.

A sea container of standard dimensions will be equipped with 100 such cylinders. The entire container will be able to store 1,400 kg of hydrogen stored at a pressure of 700 bar. The containers can be connected in series through the manufacturer's specially adapted installation, providing a large fuel buffer on board. The only limitation is the cargo capacity of the containers per ship. The number of containers needed to provide the ship's hydrogen needs is approximately 11 containers of hydrogen.

It is also necessary to install an inverter, which converts direct current into alternating current. The power station will be equipped with a transformer and electrical switchgear. The most important aspect is the possibility of installing several such inverters in one installation. The unit will be sized for hybrid operation, i.e. with batteries and the ship's power grid. Knowing the energy requirements of the ship, it is necessary to select the appropriate batteries and their capacity. The task of batteries in a ship's hydrogen system is mainly to secure the ship in electricity in the event of a total failure of the fuel cells. In addition, the batteries will compensate for temporary energy requirements.

The voltage that the fuel cells will generate is 650 VDC, so the 12-volt batteries will be connected in series, resulting in a summation of voltages while maintaining the original capacity. In order to extend the life of the batteries, their capacity should be doubled to avoid deep discharge. Connecting 54 batteries in series will result in a rounded 650 volts.

Most of the hydrogen system's equipment can be installed in place of existing ship power plant equipment. The main problem is hydrogen transportation and storage. Unfortunately, the HFO and MDO fuel tanks will be redundant after conversion. They can then serve as additional ballast tanks, or in the future with the development of the hydrogen storage system converted to hydrogen storage tanks.

A major advantage of the solution of the hydrogen system on a ship is the possibility of expansion and continuous modification of the system. If the type of use of the ship changes and the energy demand of the ship increases, the energy potential of the installation can easily be increased by adding hydrogen tanks, fuel cell modules, batteries, inverters and electric motors one by one.

# *Economic analysis*

For the economic analysis, among other things, a comparison was made between fuel costs, namely light diesel and hydrogen. For diesel fuel, costs related to  $CO_2$  emissions were also added. Further analysis focused on the aspect of converting a ship from conventional propulsion to alternative propulsion. The article analyzes selected environmental aspects, particularly those related to hydrogen, production and its application as a fuel. To this end, methods of producing hydrogen and their environmental impact were compared.  $CO<sub>2</sub>$  emissions from burning fossil fuel and  $CO<sub>2</sub>$ emissions from hydrogen production, storage and transportation were calculated. Additional costs were added to the price of diesel fuel due to CO<sub>2</sub> emissions as a fossil fuel, while the use of hydrogen for ship propulsion, regardless of the method of production, does not involve such charges.

The economic analysis of the transformation of a ship from conventional propulsion to hydrogen propulsion poses quite significant problems. Unfortunately, the total cost of such a conversion is not known at the moment. The construction of a conventionally powered Panamax-type bulk carrier costs about \$30 million (according to the price list for bulk carriers in force according to the date of access) [44]. By analogs to existing means of transport and far-reaching simplification, it can be assumed that the construction of such a hydrogen-powered vessel may cost the shipowner about \$60 million. The estimated total cost during the 10-year operation of the vessel, depending on the chosen solution, is presented in Table 4. From

**Table 4.** Comparison of costs during the ten-year operation of the vessel

Type of fuel used to propel the ship	Estimated cost [mln \$]	CO <sub>c</sub> emissions [t]
Conventional drive (low-sulfur fuel)	66	261746
Alternative propulsion (hydrogen)	30	226512
Alternative drive (conversion)	30	

the data in the table, it can be deduced that if the ship is 15 years old and has 10 years left to scrap, the cost of operation is similar. This is because the cost of conventional fuel along with  $CO_2$  emission fees will be similar to the cost of rebuilding and then operating a hydrogen-powered ship. One must also take into account that the cost of conversion is an estimate, in addition to the fact that over the next few years the price of diesel fuel will increase and hydrogen will decrease, as cheaper methods of producing it develop. Despite hydrogen being produced primarily from natural gas,  $CO_2$  emissions are still 14% lower than those from burning fossil fuels. Of course, developing non-fossil fuel methods of hydrogen production will make these emissions even lower. To fully assess the sensibility of converting a ship to alternative propulsion, it is also necessary to consider the depreciation costs of both a conventionally propelled ship and a ship with a new propulsion system. As for conventional propulsion, the basic depreciation rate for floating fleets is 7% per year [45], while there is no depreciation data for marine vessels, as it is only in the development stage.

As can be inferred from the above analysis, this conversion is not too challenging or problematic from a technical point of view. Certainly, the adaptation of a several-yearold bulk carrier to a hydrogen fuel cell system requires a great deal of work and numerous structural changes. In addition, and very importantly from the point of view of the function performed by the ship, it will be necessary to arrange one hold for containers with stored hydrogen. With the ship's lifespan averaging about 20–25 years, it is currently unknown whether this conversion will be economically justified, as this depends mainly on fuel prices. Environmentally, the conversion makes sense, because even for hydrogen derived from natural gas,  $CO_2$  emissions will be lower. In general, a ship of this size and purpose should be designed with a hydrogen system in mind at the very beginning of its design. Otherwise, the cost of adaptation and the amount of work unfortunately, but may be commensurate with the revenue the ship can generate.

The ship-owner should decide which of the emission reduction methods presented in the article is the optimal solution. The choice of one of them should be influenced by, among others: the route covered by that vessel, environmental conditions, the ability to adjust the structure, the age of the ship, and in the case of hydrogen fuel, the availability of fuel. In addition to the main advantage which is to reduce the emission of toxic compounds to the atmosphere, ship conversion has some disadvantages, mainly of a financial nature, that ship-owners should take into account.

# **CONCLUSIONS**

The purpose of the above work was to analyze the feasibility of using a hydrogen fuel cell to propel a Panamax-type bulk carrier sailing in the ECA special control zone. The proposed solutions have considerable energy and environmental potential, which in the not-so-distant future may find wide application in both the marine and industrial sectors.

ECA zones already have strict rules regarding the combustion of heavy fuels, and these rules will become increasingly stringent in the future. The installation of hydrogen on ships in the future may become an everyday occurrence due to its environmental as well as economic aspects.

Adapting a bulk carrier that is several years old to a hydrogen fuel cell system requires an enormous amount of work, numerous structural changes, and the arrangement of one cargo hold for containers with stored hydrogen. Given that the ship's lifespan averages about  $20\div 25$  years, this procedure may not be economically justified. Ideally, a ship of this size and purpose should be equipped with a hydrogen system from the beginning of construction. Otherwise, the cost of adaptation and the amount of work unfortunately may prove to be disproportionate to the revenue the ship can generate.

The cost of operating the vessel will be similar, as the purchase price of conventional fuel plus  $CO<sub>2</sub>$ emission fees will be similar to the cost of converting and then operating a hydrogen-powered vessel.

Based on current trends, it can be concluded that in the long run, the operation of a hydrogenpowered ship will be lower than that for a conventionally powered ship, as the price of diesel fuel and  $CO_2$ -related allowances will increase in the coming years, while hydrogen will decrease especially with the development of cheaper methods of producing it.

Considering that hydrogen is currently produced primarily from natural gas,  $CO_2$  emissions are still 14% lower compared to those resulting from burning fossil fuel. Of course, developing non-fossil fuel methods of hydrogen production

will make these emissions even lower. Despite the aforementioned disadvantages of converting to hydrogen propulsion on a seagoing vessel, hydrogen technology is becoming increasingly popular and attractive. The environmental benefits of this conceptual design are crucial for the entire industry, which is why all major maritime companies are intensively developing their offerings because they see the potential that exists in hydrogen.

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