

Prediction of gas holdup in the three-phase fluidized bed: air/Newtonian and non-Newtonian liquid systems

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The application of the three-phase fluidization technology in wastewater treatment and other biochemical processes has been regularly addressed in the past decades. For the design and development of the three-phase fluidized bed reactors, knowledge of the hydrodynamic parameter such as gas holdup is essential and hence in this paper an attempt has been made to study the effect of fundamental and operating variables on gas holdup. On the basis of the experimental results, a unified correlation has been developed to predict gas holdup in the fluidized bed using the Newtonian and the non-Newtonian liquids. The experimental results showed good agreement with those predicted according to the developed correlation.

Keywords: Gas holdup, fluidized beds, non-Newtonian liquids, multiphase reactors, hydrodynamics.

INTRODUCTION

During the recent years the three-phase fluidized beds have emerged as one of the most promising devices for the applications in many industrial processes such as coal liquefaction, catalytic hydrogenation and desulphurization of petrochemicals, Fischer-Tropsch synthesis, biochemical fermentation and biological waste water treatment processes, polymerization processes, etc. The three-phase fluidized bed is preferred in many industries because of simple design and construction, high mass transfer rates as a result of good mixing¹⁻⁵. Now it has gained importance in biotechnology also, where bacteria or enzymes are entrapped within porous particles or immobilized on the surface of the inert solids⁴⁻⁷. The successful scale up, design and operation of the fluidized beds mainly depend on the accurate prediction of the behavior and features of the system such as gas holdup. Over the years, many significant contributions have been made by investigators towards gas holdup in fluidized beds⁸⁻¹⁶. Mostly Newtonian liquids were used to develop the correlations for the prediction of gas holdup^{11-13,17}. The use of non-Newtonian liquids for the prediction of gas holdup has been done only on a limited scale¹⁷⁻²⁰. Since most of the industrial effluents behave as power law fluids, there is a vital need to obtain data with a wide range of variables using non-Newtonian liquids and to develop a generalized correlation to represent the data^{4,5,15,18,19,21}. Since many biochemical reaction fluids behave as power law non-Newtonian liquids, an attempt has been made to study the effect of fundamental and operating variables on gas holdup, and also to develop a unified correlation for the estimation of gas holdup using the Newtonian and the non-Newtonian liquids.

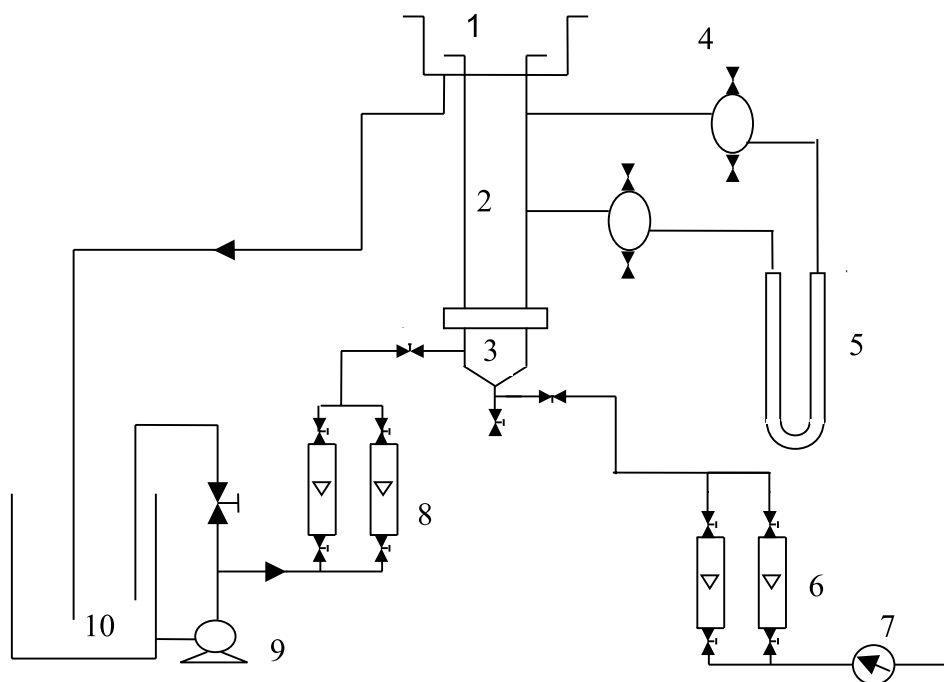
EXPERIMENTAL SETUP AND PROCEDURE

All experiments were carried out in a Perspex column (0.15 m inner diameter and 1.8 m height) as shown in Fig. 1. The details of the experimental apparatus can be found elsewhere^{3,22}. The details of the properties of the solids and fluids used in the present study are given in Table 1.

Water, different concentrations of glycerol (lab grade and commercial grade), butyric acid and Mono Ethanol Amine (MEA) were Newtonian liquid systems and different concentrations of Carboxy Methyl Cellulose (CMC), were the non-Newtonian liquids and 12 different particles were used. The experimental column had a provision to feed the gas and liquid at the bottom of the column. Compressed air was fed into the bottom of the column through a pressure regulating valve. A gas distributor was provided at the bottom of the fluidized column, whereas, a gas-liquid separator was provided at the top of the fluidized column. The gas-liquid distributor is designed in such a way that uniformly distributed gas and liquid mixtures entered the fluidized column. The distributor section was made up of conical Plexiglas of 0.3 m in height, had a divergence angle of 4.5°. The higher cross section end was fitted to a testing section, with a perforated plate made of perspex sheet of 0.001 m thick, 0.15 m diameter having the opening area of approximately 20% of the column area in between covered with 20 mesh stainless steel screen at the top. 0.0008 m diameter holes in triangular pitch were made in 15 circles of nearly 0.005 m gap from the centre. After attaining a steady state condition, air and liquid flow rates were suddenly stopped by closing both the valves simultaneously and gas holdup was measured^{14,19}. The experimental results were randomly checked and it was found that the reproducibility of the errors was within $\pm 2\%$. The equivalent volume diameter of non spherical particles has been calculated by using the following formula:

$$\frac{\pi d_p^3}{6} = \text{Volume of one non-spherical particle}$$

Where d_p spherical volume equivalent diameter, which is the diameter of a sphere whose volume is the same as that of the solid volume of non spherical particle. Shear stress and shear rate were calculated using Brookfield Rheometer (model LVDV- II+). By plotting shear stress versus shear rate, the flow consistency index (k) and fluid behaviour index (n) were calculated.



1. Disengagement section 2. Testing section 3. Claming section 4. Gas-liquid separators 5. Manometers 6. Gas rotameters 7. Pressure regulating valve 8. Liquid rotameters 9. Circulating pump 10. Liquid storage tank

Figure 1. Schematic of the experimental setup

Table 1. The details of the particles and liquid system used in this work

Bed Characteristics		d_p / mm	$\rho_s / \text{kg m}^{-3}$	ϕ_s	D / mm
Particle 1	Spheres	1	2480	1	150
Particle 2	Spheres	2	2480	1	150
Particle 3	Spheres	4	2480	1	150
Particle 4	Spheres`	5.5	2480	1	150
Particle 5	Spheres	7.2	2480	1	150
Particle 6	Spheres	10.36	2114	1	150
Particle 7	Berl Saddles	4.8	2050	0.33	150
Particle 8	Berl saddles	6.58	2213	0.33	150
Particle 9	Berl saddles	11.5	2456	0.33	150
Particle 10	Raschig Rings	5.1	2480	0.58	150
Particle 11	Raschig Rings	3.51	2173	0.58	150
Particle 12	Raschig Rings Rings	13.66	2083	0.58	150
Properties of Fluids		$\rho_l / \text{kg m}^{-3}$	$\mu_l / \text{kg m}^{-1} \text{s}^{-1}$		
			$\text{K/kg m}^{-1} \text{s}^{-2}$	n	$\sigma_l / \text{Nm}^{-1}$
System 1	Water	1000	0.00085	1	0.072
System 2	$\varphi = 20\%$ glycerol (commercial grade)	1010	0.002	1	0.069
System 3	$\varphi = 60\%$ glycerol (commercial grade)	1020	0.006	1	0.069
System 4	$\varphi = 90\%$ glycerol (commercial grade)	1040	0.01	1	0.068
System 5	$\varphi = 65\%$ glycerol (lab grade)	1158	0.019	1	0.069
System 6	$= 85\%$ glycerol (lab grade)	1185	0.032	1	0.068
System 7	MEA	1050	0.015	1	0.045
System 8	Butyric acid	1010	0.001	1	0.039
System 9	$w = 0.1\%$ CMC	1020	0.0084	0.92	0.072
System 10	$w = 0.5\%$ CMC	1020	0.0184	0.88	0.071
System 11	$w = 1\%$ CMC	1020	0.0550	0.86	0.069

RESULTS AND DISCUSSION

The experimentally measured gas holdup values obtained in the present study have been analyzed for their dependency on the fundamental and operating variables

such as superficial gas and liquid velocities, size and shape of the solid particles, physical and rheological properties of the fluids. From the experimental results, it was observed that both the superficial gas and liquid velocities

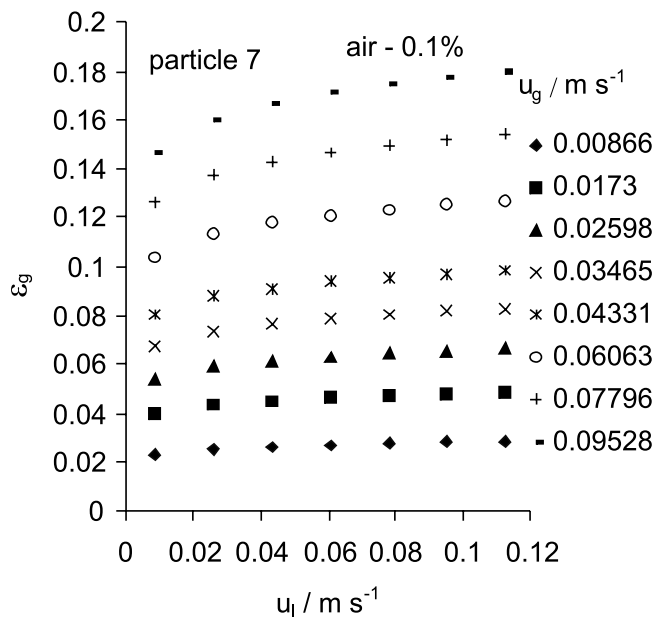


Figure 2. The effect of liquid and gas velocities on gas holdup

had a significant effect on gas holdup. Fig. 2 shows the variation in the gas holdup with respect to superficial liquid and gas velocities for the particle size (d_p) of 4.8 mm for air-0.1% CMC system. The gas holdup increased with an increase in gas velocity for a constant liquid flow rate. The same trend was observed in previous studies^{4, 6, 23}. However, the increase of gas holdup with an increase of liquid velocity is not significant at low superficial gas velocities whereas at higher superficial gas velocities gas holdup was increased slightly. This trend coincides with the results published by the previous authors^{18, 19}. The effect of particle size on gas holdup is shown in Fig. 3 for air-water system. It was observed that there is a decrease in gas holdup with an increase in particle diameter, which is mainly due to increasing the bubble breakage. The same trend is in agreement with the published literature results²⁰. The influence of the sphericity of particle on gas holdup is shown in Fig. 4, from which it is observed that an increase of the sphericity of particle decreases the gas holdup and it is mainly due to decreasing the surface area per unit volume of particle which leads to less bubble

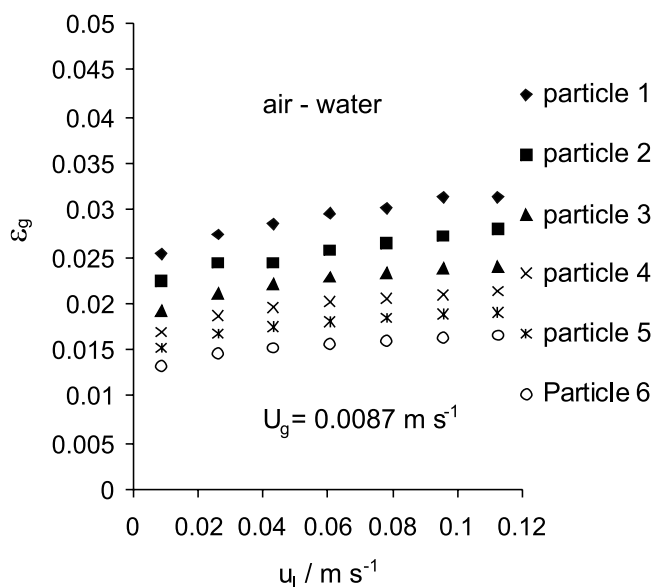


Figure 3. The effect of particle diameter on gas holdup

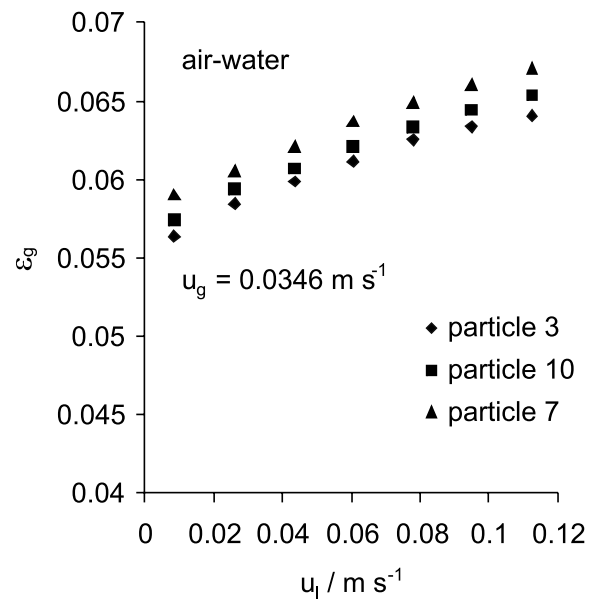


Figure 4. The effect of the sphericity of particle on gas holdup

breakage. The dependency of the gas holdup on liquid properties was analyzed using 11 different liquid systems. At constant liquid flow rate, gas holdup increases with increasing liquid viscosity, as shown in Figure 5. The same trend is also observed with an increasing flow consistency index (k) for non-Newtonian fluids (Fig. 6). Increasing the liquid viscosity/consistency index enhances the bubble breakages and hence the gas holdup increases¹⁸.

The present experimental data and literature data^{6, 10, 14, 18, 19, 24, 25} were analyzed using the available literature correlations (Table 2). Begovich and Watson correlation 4 predicted good results with the data of Bloxom et al.,¹⁰ Miura and Kawase¹⁸ and Miura et al.¹⁹ with the minimum AARD limits (less than 13% AARD) but failed to comply with the rest of the data sets^{6, 14, 24, 25} (more than 25% AARD). The reason could be that the effective physical properties of liquids and particle dimensions were not properly accounted for in the development of the correlation. The present experimental and literature data, when tested with the Parulekar and Shah¹¹

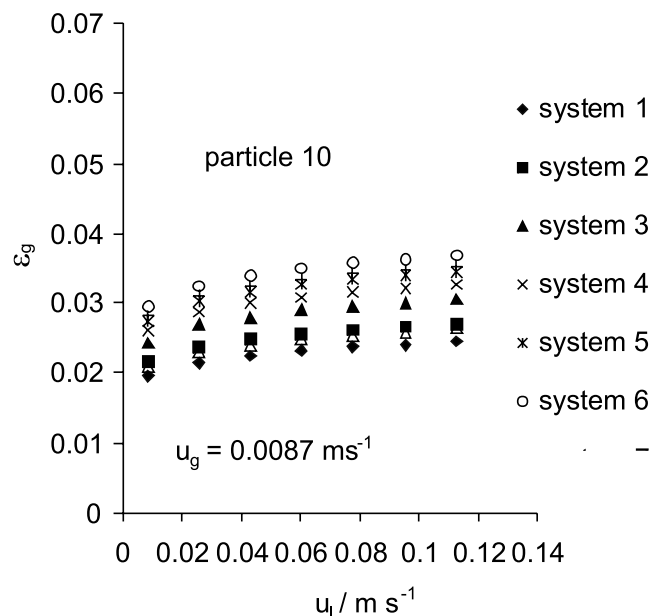
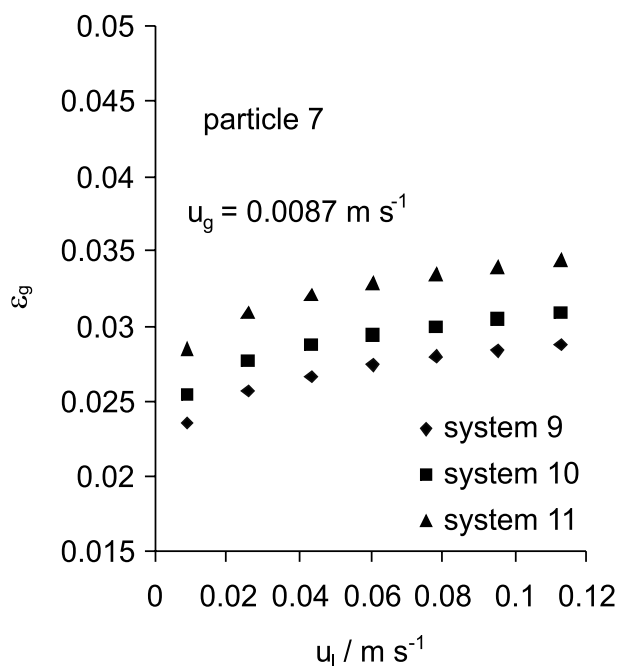


Figure 5. The effect of physical properties of liquids on gas holdup

Table 2. A list of important literature correlations for gas holdup

Author	Correlations	System	Range of variables
Begovich and Watson ⁴	$\varepsilon_g = 0.048(u_g)^{0.72} d_p^{0.168} (D)^{-0.125}$	Air – water	$d_p=0.0046-0.0062\text{m}$ $\rho_s=1720-2440\text{ kg/m}^3$ $u_g=0-0.173\text{ m/s}$ $u_l=0-0.12\text{ m/s}$ $D=0.0762\ \&\ 0.152\text{ m}$
Parulekar and Shah ¹¹	$\varepsilon_g = 0.0866 \left(\frac{1}{\sigma_l} \right)^{0.01} U_g^{0.5} D^{-0.08}$	Hydrogen-oil	$d_p=0.00005-0.000275\text{ m}$ $\rho_s=1300\text{ kg/m}^3$ $\rho_l=900\text{ kg/m}^3$ $u_g=0-0.030\text{ m/s}$ $u_l=0.00075-0.003\text{ m/s}$ $D=0.08-0.16\text{ m}$
Khang et al. ¹²	$(1 - \varepsilon_g) u_g + \varepsilon_g u_l = \varepsilon_g (22.67 \varepsilon_g + 10.44)$	Air-kerosene	$d_p=0.0011\text{m}$ $\rho_s=1330\text{ kg/m}^3$ $\rho_l=810\text{ kg/m}^3$ $\mu_l=0.0014\text{ kg/m.s}$ $u_g=0-0.0022\text{ m/s}$
Jean and Fan ¹³	$\varepsilon_g = 0.00164 u_g^{0.988} (-0.221 \times 10^{-5} u_l^2 - 0.564 u_l + 28.28)$	Air-water	$d_p=0.00033-0.006\text{ m}$ $\rho_s=2200-22876\text{ kg/m}^3$ $u_l=0.0412-0.47\text{ m/s}$ $u_g=0-0.1208\text{ m/s}$
Yu and Kim ¹⁶	$\varepsilon_g = 3.697 d_p^{0.309} u_l^{-0.0222} u_g^{0.701}$	Air- water	$d_p=0.0004-0.006\text{ m}$ $\rho_s=2500\text{ kg/m}^3$ $u_g=0.01-0.14\text{ m/s}$ $u_l=0.006-0.01\text{ m/s}$
Ramesh and Murugesan ²⁶	if $N_{Re,l} \leq 100$ $\varepsilon_g = 0.17 (Fr_g)^{0.33} (Ar_l)^{0.125} (Mo_l)^{0.05} (N_{Re,l})^{-0.065}$ if $N_{Re,l} > 100$ $\varepsilon_g = 0.11 (Fr_g)^{0.35} (Ar_l)^{0.11} (Mo_l)^{0.075} (N_{Re,l})^{0.2}$	Air-water or MEA or Glycerol (25%, 55%)	$d_p=0.00411-0.0068\text{ m}$ $\rho_s=2030-2480\text{kg/m}^3$ $u_g=0-0.13\text{ m/s}$ $u_l=0-0.13\text{ m/s}$ $\sigma_l=0.049-0.072\text{ N/m}$ $\mu_l=0.0008-0.015\text{kg/m.s}$ $\rho_l=1000-1150\text{kg/m}^3$

**Figure 6.** The effect of rheological properties of the non-Newtonian fluids on gas holdup

correlation for the prediction of gas holdup showed relatively high deviation ($>70\%$ AARD). This deviation may be attributed to the fact that even though the author had used hydrogen-oil systems, the individual physical properties of liquids and the solids were not properly taken

into account for the development of the correlation. The present and the literature data, when tested with the Khang et al.,¹² and Jean and Fan¹³ correlation, gave high AARD (more than 85% AARD). The authors studied only the influence of the gas and liquid flow rates on the gas holdup. Since the suggested correlation was developed using a restricted range of variables it gave high AARD when particles with other dimensions were considered. Yu and Kim¹⁶ correlation predicted high deviation (more than 26% AARD) for Dhanuka and Stepanek⁶, Saberian-Broudjenni et al.¹⁴, Oh and Kim²⁴, and Nacef et al.²⁵ data, compared to other available literature data of Bloxom et al.¹⁰, Miura and Kawase¹⁸ and Miura et al.¹⁹ and this was mainly due to the fact that the appropriate effects of physical properties of liquids, were not properly taken into account for the development of the correlation. Though Ramesh and Murugesan²⁶ had studied the effect of particle diameter, phase velocities and physical properties of the fluids on gas holdup, their correlation was restricted to Newtonian systems.

Graphical analysis of the present data (Fig. 2 – Fig. 6) shows that the variation of gas holdup can be attributed to the effect of all the above said variables. From the literature it is observed that most of the literature correlations were restricted to Newtonian liquid systems^{4, 11 – 13, 16, 26} and hence those could not be used non-Newtonian fluids and hence in this study, the approach of dimensionless method was adopted for the establishment of the unified gas holdup

Table 3. The details of the literature particles used for the gas holdup analysis

Bed Characteristics	Particle Diameter, d_p / mm	Particle Density, ρ_s / kg m ⁻³	Particle Sphericity, ϕ_s	Column Diameter, D / mm	Author
Spheres	4.08	2960	1	50	Dhanuka and Stepanek ⁶
Spheres	5.86	2960	1	50	
Spheres	4.62	2260	1	7.62	Bloxom et al. ¹⁰
Spheres	2.55	1380	1	52	Saberian-Broudjenni et al. ¹⁴
Alumina Extrudates	2	2160	0.78	52	
Alumina Extrudates	2	1605	0.78	52	
Spheres	3	2500	1	68	Miura and Kawase ¹⁸
Spheres	5	2500	1	68	
Spheres	7	2500	1	68	
Spheres	3	2500	1	68	Miura et al. ¹⁹
Spheres	5	2500	1	68	
Spheres	1.63	2500	1	15	Oh and Kim ²⁴
Spheres	2.92	2500	1	15	
Spheres	7.85	2500	1	15	
Spheres	1.2	2500	1	152	Nacef et al. ²⁵
Spheres	3.1	2500	1	152	
Spheres	3.5	1245	1	152	

Table 4. The details of the literature liquid systems used for the gas holdup analysis

Properties of fluids	Liquid Density, ρ_l / kg m ⁻³	Liquid Viscosity, μ_l (kg/m/s)		Liquid Surface Tension, σ_l / Nm ⁻¹	Author
		K / Kg/m/s ⁿ⁻²	n		
Water	995	0.00085	1	0.0712	Dhanuka and Stepanek ⁶
Glycerine Solution 1	1160	0.0038	1	0.064	Bloxom et al. ¹⁰
Glycerine Solution 2	1000	0.0009	1	0.07	
Glycerine Solution 3	1100	0.009	1	0.064	
Cyclohexane	775	0.001	1	0.027	Saberian et al. ¹⁴
Tetrachloroethane	1620	0.0009	1	0.032	
Kerosine	780	0.0011	1	0.025	
Water	997	0.0009	1	0.072	Miura and Kawase ¹⁸
w = 0.1 % CMC	998	0.024	0.788	0.0728	
w = 0.2 % CMC	999	0.169	0.625	0.073	
Water	997	0.0009	1	0.072	Miura et al. ¹⁹
w = 0.05 % CMC	997	0.0299	0.719	0.07	
w = 0.1 % CMC	998	0.0648	0.687	0.07	
w = 0.1% Xanthan gum	1000	0.0675	0.629	0.07	
Water	1000	0.001	1	0.072	Oh and Kim ²⁴
Water	1000	0.001	1	0.072	Nacef et al. ²⁵
φ =1% Ethanol	1000	0.001	1	0.067	

correlation for both Newtonian and non-Newtonian liquids with a wide range of operating conditions (Tables 3 – 5). The combined effects of the liquid properties of the Newtonian and the non-Newtonian fluids were accommodated using Modified Morton's number²⁷, the effects of viscous force and gravity force were combined in terms of Froude number's of fluids, the ratio of the downward to upward force, the column geometry effects and particle sphericity were considered to develop the unified present correlation. Regression analysis of the available gas holdup data yielded the following constants and indices for the equation,

$$\varepsilon_g = 0.98 (Fr_l)^{0.0438} (Fr_g)^{0.382} (Mo_{l,M})^{0.0265} (\rho_s / \rho_l)^{-0.529} (d_p / D)^{0.0339} (\phi_s)^{-0.0217} \quad (1)$$

Statistical error analysis of the proposed correlation (Eqs. (1)) showed an AARD of 10.5% for gas holdup indicating a satisfactory representation of the available

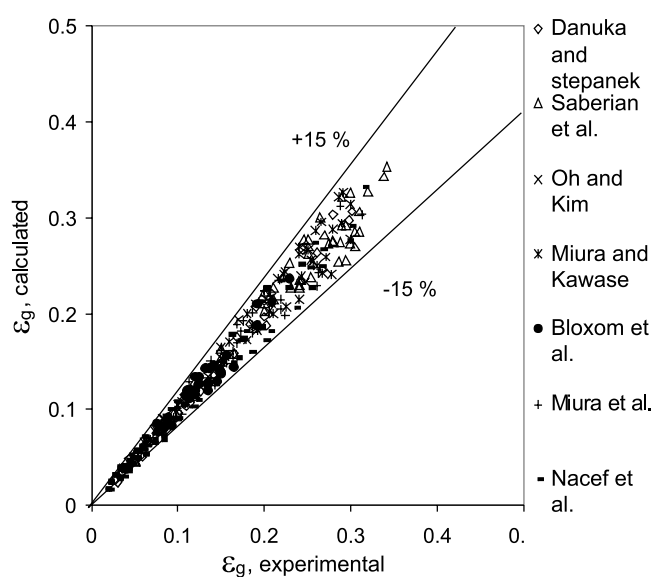
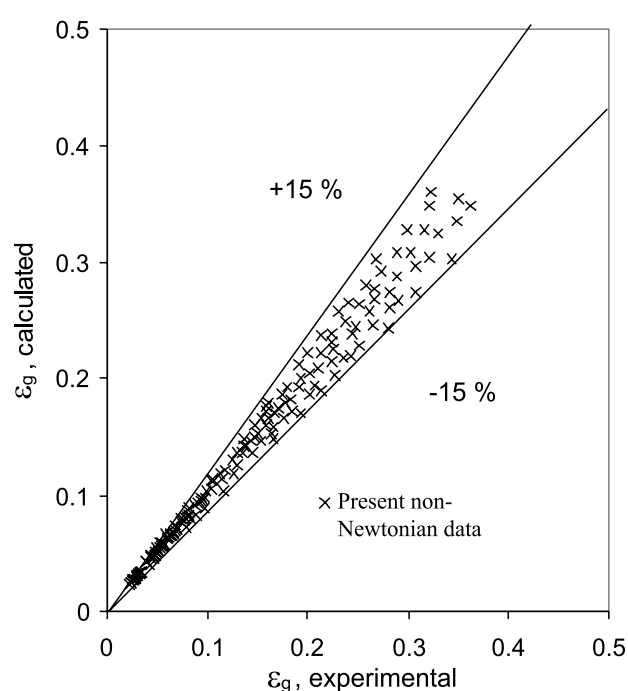
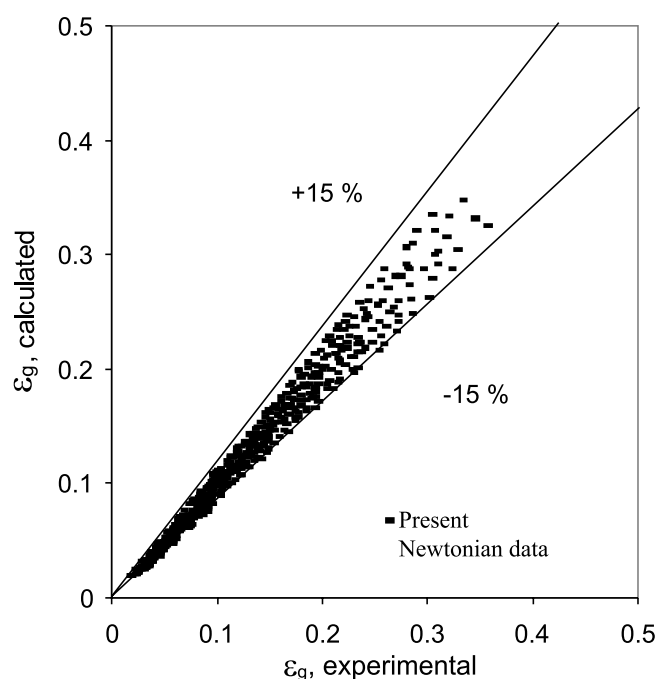
Table 5. A range of variables used for the development of the proposed correlation

S.No.	Variable	Range of variable used
1.	Superficial gas velocity (u_g)	0.00375-0.1375 m/s
2.	Superficial liquid velocity(u_l)	0.008-0.2487 m/s
3.	Particle diameter (d_p)	0.001-0.01366 m
4.	Sphericity of the particle (ϕ_s)	0.33-1.0
5.	Particle density (ρ_s)	1245-2960 kg/m ³
6.	Column diameter (D)	0.005-0.15 m
7.	Liquid density (ρ_l)	995-1620 kg/m ³
8.	Liquid viscosity (μ_l)	0.00085-0.032 kg/m/s
9.	Fluid consistency index (k)	0.00085-0.169 kg/m/s ²⁻ⁿ
10.	Flow behaviour index (n)	0.625-1.0
11.	Liquid surface tension (σ_l)	0.025-0.072 N m ⁻¹

data for the air-Newtonian and the air-non Newtonian systems. The statistical analysis of the proposed and available literature correlations for the present and literature

Table 6. Statistical comparison of gas holdup with the present and literature data

Correlations	Present data		Dhanuka & Stepanek ⁶		Bloxom et al. ¹⁰		Saberian-Broudjenni et al. ¹⁴		Miura and Kawase ¹⁸		Miura et al. ¹⁹		Oh and Kim ²⁴		Nacef et al. ²⁵	
	AARD %	Bias	AARD %	Bias	AARD %	Bias	AARD %	Bias	AARD %	Bias	AARD %	Bias	AARD %	Bias	AARD %	Bias
Begovich and Watson ⁴	19.5	1.06	24.1	0.81	13.55	0.89	42.4	1.7	8.9	1.05	9.02	0.92	78.6	0.64	27.6	1.3
Parulekar and Shah ¹¹	129.4	0.54	127.1	0.45	85.5	0.61	17.2	0.93	43.3	0.7	65.1	0.61	159.3	0.4	87.4	0.56
Khang et al. ¹²	306.1	0.32	799.8	0.12	185.8	0.35	44.6	0.7	131.5	0.44	149.7	0.4	392.6	0.21	177.9	0.38
Jean and Fan ¹³	94.3	0.54	9.4	1.06	144.2	0.41	50.3	0.73	115.3	0.48	157.8	0.39	135.3	0.45	43.9	0.75
Yu and Kim ¹⁶	25.8	1.1	24.6	1.3	5.95	1.01	55.5	2.27	17.5	1.2	6.5	1.06	48.7	0.89	30.5	1.4
Ramesh and Murugesan ²⁶ $N_{Re} \leq 100$	26.4	1.30	–	–	10.66	1.1	47.5	1.92	29.3	1.42	15.5	1.1	22.2	1.28	35.9	1.60
Ramesh and Murugesan ²⁶ $N_{Re} > 100$	22.3	1.06	15.6	0.93	11.9	1.1	45.9	1.83	23.1	1.31	12.6	1.1	45.8	0.82	37.1	1.52
Present Eq (1)	10.5	1.01	14.8	1.3	14.77	0.91	13.7	1.2	14.6	1.06	13.8	1.02	11.8	1.01	14.8	1.04

**Figure 7.** Comparison of the literature data vs. the calculated gas holdup using the present correlation**Figure 9.** Comparison of the present experimental non-Newtonian data vs. calculated gas holdup using the present correlation**Figure 8.** Comparison of the present experimental Newtonian data vs. calculated gas holdup using the present correlation

data were shown in the Table 6. The validity of the present correlation has been tested with the available experimental literature gas holdup data and AARD found to be within 15%, which shows a satisfactory agreement (Figs. 7 – 9).

CONCLUSION

In the present work, a careful analysis of the effect of the fundamental and operating variables on gas holdup has been studied in a three-phase fluidized bed using various Newtonian and non-Newtonian liquids. The experimental results indicate that the gas holdup increases with increased gas flow rate; viscosity of the liquid and flow consistency index whereas gas holdup decreases with increased particle diameter. The unified correlation for the estimation of gas holdup in a three-phase fluidized bed was developed using literature and the present data covering a wide range of variables. The statistical error analysis of the proposed correlation showed an AARD of 10.5 % for gas holdup indicating a satisfactory represen-

tation of the available data for the air-Newtonian and the air-non Newtonian systems. The validity of the present correlation has been tested with the available experimental literature gas holdup data and AARD found to be within 15%, which shows a satisfactory agreement and also the graphical analysis showed that the predictive ability of the present proposed correlation is good. Therefore, the proposed correlation can be confidently used for the estimation of the gas holdup, with the knowledge of the fundamental and operating variables.

Symbols used

$$\text{AARD} = \frac{1}{N} \sum_{i=1}^N \left| \frac{(\text{experimental} - \text{calculated})}{\text{experimental}} \right|, [-]$$

$$\text{Bias} = \exp \frac{1}{N} \sum_{i=1}^N \ln \frac{\text{experimental}}{\text{calculated}}, [-]$$

D	– column diameter, [m]
d_p	– particle diameter, [m]
Fr_g	– Froude number of gas, $u_2^2 g^{-1} d_p^{-1}$
Fr_l	– Froude number of liquid, $u_1^2 g^{-1} d_p^{-1}$
g	– acceleration due to gravity, [m s^{-2}]
K	– flow consistency index, [$\text{kg m}^{-1} \text{s}^{-n}$]
L	– length of the non-spherical particles, [m]
$Mo_{L,M}$	– modified Morton number of liquid, $d_p^{4(1-n)} u_1^{4(n-1)} g k^4 \sigma_l^{-3} \rho_l^{-1}$, [-]
N	– number of data points, [-]
n	– fluid behavior index, [-]
u_g	– superficial gas velocity, [m s^{-1}]
u_l	– superficial liquid velocity, [m s^{-1}]
w	– mass fraction, %

Greek letters

ρ_l	– liquid density, [kg m^{-3}]
σ_l	– liquid surface tension, [N m^{-1}]
μ_l	– liquid viscosity, [$\text{kg m}^{-1} \text{s}^{-1}$]
ρ_s	– particle density, [kg m^{-3}]
ε_g	– gas holdup, [-]
ϕ	– sphericity of the particle, [-]
ρ_g	– gas density, [kg m^{-3}]
μ_g	– gas viscosity, [$\text{kg m}^{-1} \text{s}^{-1}$]
φ	– volume fraction, %

Abbreviations

AARD	– absolute average relative deviation
CMC	– carboxy methyl cellulose
MEA	– mono ethanol amine

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