

Salt effect on the enthalpy of mixing of 2-propanol + acetic acid at 303.15 K

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This paper presents the effect of two dissolved inorganic salts (zinc chloride, ZnCl₂ and ammonium chloride, NH₄Cl) on the enthalpy of mixing (H^E) of 2-propanol + acetic acid binary system measured at 303.15 K using an isothermal displacement calorimeter with vapour space. A decreasing trend in the excess enthalpy of mixing values in the presence of ZnCl₂ and NH₄Cl indicate the endothermic behavior of this system. The Redlich-Kister equation has been used to fit the experimental H^E data. The deviations from the ideal value and binary parameters were calculated and reported.

Keywords: Excess enthalpy, binary system, salt effect, 2-propanol, acetic acid.

INTRODUCTION

The excess thermodynamic properties of binary liquid mixtures are important to understand and interpret the nature of interactions between the molecules of the mixtures. Excess thermodynamic functions have been used as a qualitative guide to predict the extent of complex formation in binary liquid mixtures. Furter and Cook¹ and Jacques and Furter² have studied the influence of the added salt on the relative volatilities of two liquid components using 19 inorganic salts. The formation of the associated complexes or clusters of molecules of the volatile component around salt ions and its effect on relative volatilities have been studied extensively by Long and Mc Devit³. The salt effect is also believed to be a complex function of salt + solvent interaction and self-interaction among the system components⁴. As the equation derived by Sada et al.⁵ indicated the changes in the chemical potential of the solvent components when a salt is added to a solvent mixture.

Properties like relative volatility and azeotrope are influenced by the addition of salts. Meranda and Furter⁶ have observed the gradual shift in the azeotropic composition in certain azeotropic systems by the addition of salts. Certain salts have been found to completely eliminate the azeotrope. Therefore, it is of greater interest to investigate the effect of dissolved salts on the enthalpy of mixing of liquid mixtures which are of commercial importance. Since there is an interrelation between the excess free energy and the excess enthalpy of liquid mixtures, a few researchers^{7,8} have studied the effect of added salts on the excess enthalpy values of liquid mixtures along with notable contributions from our group⁹⁻¹⁶. In this investigation, the effect of two dissolved inorganic salts, namely zinc chloride and ammonium chloride on the enthalpy of mixing values of 2-propanol + acetic acid binary system has been studied experimentally.

EXPERIMENTAL SECTION

Analytical reagent grade 2-propanol, acetic acid, and the salts (zinc chloride and ammonium chloride) used in this investigation were supplied by E-Merck. The solvents were purified by fractional distillation; the physical properties of the solvents (density, ρ ; boiling point, T_b) and the

salts (melting point, T_m) used in this study were found to be almost identical to the literature values¹⁷ as shown in Table 1. Their densities were measured using a bicapillary pycnometer and their boiling points were measured using an ebulliometer giving a precision of ± 0.2 K. The salts were dried before use, and their melting point and purity (%) values were received from the supplier.

Table 1. The physical properties of the solvents and salts used

solvent	this work	Ref. 17
	boiling point, T_b /[K]	
2-propanol	355.2	355.3
acetic acid	390.6	390.9
	density, ρ /[g·cm ⁻³] at 298.15 K	
2-propanol	1.8010	1.8030
acetic acid	1.0491	1.0492
salt	(as reported by the supplier)	
	melting point, T_m /K	purity
zinc chloride	566.35	≥ 99.9 %
ammonium chloride	612.85	≥ 99.9 %

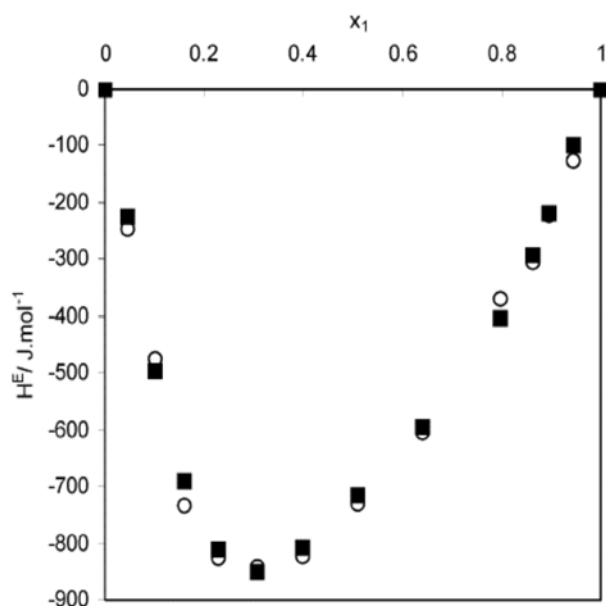
Preparation of the salt solutions, experimental procedures and the apparatus set-up adopted in this work has been reported in our previous paper^{15,16} and elaborated briefly in this section. The concentrations of the salts reported in this work [(5 and 10) %] are the initial concentrations by mass [mass of salt/(mass of salt + mass of solvent)] before mixing with the other solvent. The performance of the calorimeter and its reliability for the measurement of the enthalpy of mixing values were ascertained by determining the enthalpy of mixing values of the non-salt water + methanol binary system at 303.15 K (Figure 1), and the data compared well (within 2%) with the literature data¹⁸. Triplicate samples were prepared for each 2-propanol + acetic acid composition (refer to the varying mole % of 2-propanol (x_1) values given in Tables 2 and 3) to ensure reproducibility (within ± 3 %), and the average values are presented. The mole fraction of acetic acid can be referred to as x_2 whereas x_3 refers to the mole fraction of solute (in Tables 2 and 3), and the sum of $x_1 + x_2 + x_3$ is equal to one.

Table 2. Enthalpy of mixing the data for the system 2-propanol + acetic acid at 303.15 K for the salt ZnCl_2

no salt			5% ZnCl_2			
x_1 [mol%]	H^E_{exptl} [$\text{J} \cdot \text{mol}^{-1}$]	H^E_{calcd} [$\text{J} \cdot \text{mol}^{-1}$]	x_1 [mol%]	x_3 [mol%]	H^E_{exptl} [$\text{J} \cdot \text{mol}^{-1}$]	H^E_{calcd} [$\text{J} \cdot \text{mol}^{-1}$]
0.122	149.0	142.8	0.097	7.43×10^{-2}	589.6	590.2
0.205	426.5	420.8	0.15	6.41×10^{-2}	836.1	841.2
0.286	747.0	758.2	0.229	5.72×10^{-2}	1040.7	1032.1
0.391	1177	1204	0.299	3.98×10^{-2}	1210.1	1201.5
0.446	1440	1410.4	0.405	3.09×10^{-2}	1360.5	1295.2
0.582	1760	1746.5	0.409	1.92×10^{-2}	1490.2	1482.1
0.684	1751	1764.2	0.650	1.23×10^{-2}	1569.9	1574.2
0.798	1472	1483.4	0.799	4.18×10^{-3}	1479.1	1581.2
0.912	890.0	805.8	0.896	1.32×10^{-3}	1068.5	1062.1

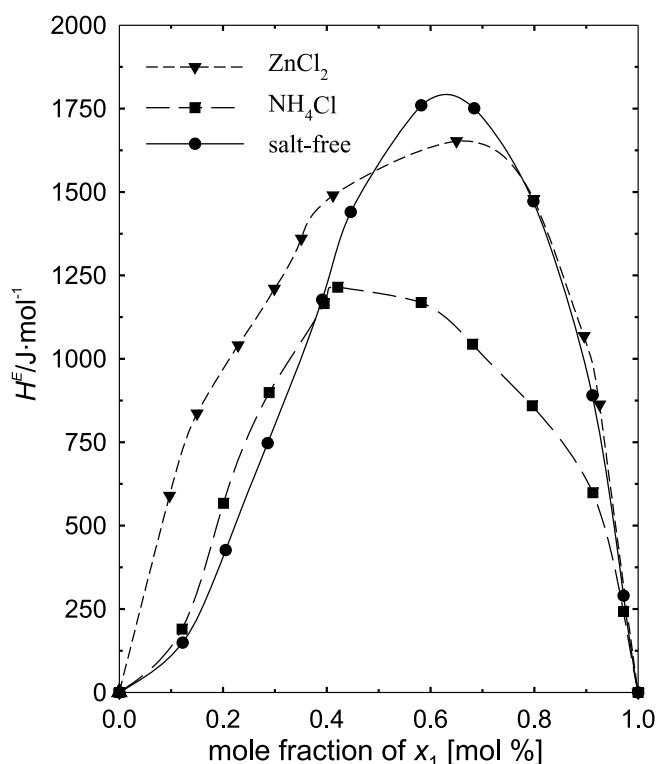
Table 3. Enthalpy of mixing the data for the system 2-propanol + acetic acid at 303.15 K for the salts ZnCl_2 and NH_4Cl

10% ZnCl_2				5% NH_4Cl			
x_1 [mol%]	x_3 [mol%]	H^E_{exptl} [$\text{J} \cdot \text{mol}^{-1}$]	H^E_{calcd} [$\text{J} \cdot \text{mol}^{-1}$]	x_1 [mol%]	x_3 [mol%]	H^E_{exptl} [$\text{J} \cdot \text{mol}^{-1}$]	H^E_{calcd} [$\text{J} \cdot \text{mol}^{-1}$]
0.130	7.66×10^{-2}	981.2	988.3	0.121	3.92×10^{-2}	189.6	193.3
0.189	6.51×10^{-2}	1213.2	1199.3	0.201	2.92×10^{-2}	567.1	551.4
0.287	5.16×10^{-2}	1411.2	1415.6	0.289	2.15×10^{-2}	898.6	912.9
0.376	4.00×10^{-2}	1550.1	1550.3	0.395	1.59×10^{-2}	1165.9	1168.8
0.44	3.10×10^{-2}	1610.1	1625.5	0.450	1.21×10^{-2}	1214.6	1215.3
0.579	1.96×10^{-2}	1700.2	1678.9	0.582	6.98×10^{-3}	1168.9	1155.3
0.682	1.19×10^{-2}	1590.2	1540.4	0.681	4.62×10^{-3}	1043.7	1039.3
0.782	6.20×10^{-3}	1161.2	1203.3	0.796	2.71×10^{-3}	859.3	884.6
0.910	1.71×10^{-3}	536.5	515.0	0.913	1.27×10^{-3}	598.6	579.0
0.972	1.33×10^{-4}	150.2	149.8	0.972	6.27×10^{-5}	242.6	240.1

**Figure 1.** Enthalpy of mixing of water + methanol at 303.15 K: O, this work; ■, Battler and Rowley¹⁸

RESULTS AND DISCUSSION

The experimental excess enthalpy data obtained for the 2-propanol + acetic acid system under various salt conditions are given in the Tables 2 and 3 and also represented graphically in Figures 2 and 3. Both 2-propanol and acetic acid are polar protic solvents. The salts chosen in this study are ZnCl_2 (5 and 10 wt %) and NH_4Cl (5 wt %). Acetic acid possesses more solvating power than 2-propanol, and the salts are more freely soluble in acetic acid than in 2-propanol. The enthalpy of mixing of the salt-free system is endothermic. This is quite obvious from the fact that, within acetic acid, there are strong

**Figure 2.** Effect of addition of 5% mass of salts, ZnCl_2 (▼); NH_4Cl (■) and salt-free solution (●) on the enthalpy of mixing (H^E) of 2-propanol + acetic acid at 303.15 K against the mole fraction of x_1 . Solid lines and symbols indicate the calculated and experimental H^E values, respectively

intermolecular forces due to hydrogen bonding. The presence of carboxyl group assists intermolecular binding through both carboxyl and OH groups. In comparison, 2-

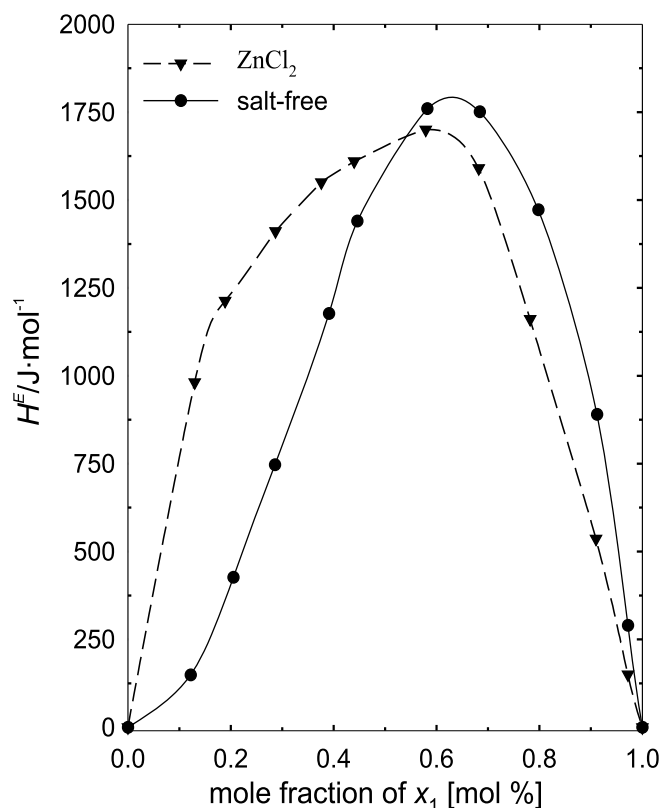


Figure 3. The effect of an addition of 10% mass of the salt ZnCl_2 (\blacktriangledown) and salt-free solution (\bullet) on the enthalpy of mixing (H^E) of 2-propanol + acetic acid at 303.15 K against the mole fraction of x_1 . The solid lines and symbols indicate the calculated and experimental H^E values, respectively

propanol is weakly associated. Although alcoholic OH aids intermolecular association through hydrogen bonding, the large alkyl group disfavors enhanced molecular association. Hence, the weakly associated 2-propanol in the presence of the strongly associated acetic acid exhibits endothermic excess enthalpy values.

The influence of the added salts on the separation feasibility of 2-propanol + acetic acid system is evaluated from Figures 2 and 3. The salts used in the present study differently alter the magnitude of endothermic excess enthalpy in the region of low and high mole fraction of 2-propanol (referred to as x_1 in Figures 2 and 3). In the region of lower mole fraction of 2-propanol, an increase in the H^E values with the added salts was observed and the reverse trend was observed in the region of high mole fraction. Hence, the phase separation in 2-propanol + acetic acid system is expected to be difficult even in the presence of salts if the mole fraction of 2-propanol is less. On the other hand, phase separation becomes easier with higher mole fraction of 2-propanol. During the actual process of separation of two components by distillation, it would be more beneficial if the mole fraction of 2-

propanol in the pot residue is maintained at around 0.5 in the presence of any of the chosen salts. Among the salts examined, NH_4Cl largely favor phase separation compared to ZnCl_2 . The influence of the salts ZnCl_2 and NH_4Cl on the excess enthalpy of mixing of this system under different salt concentration is illustrated in the Tables 2 and 3.

Data Correlation and Statistical Analysis

The Redlich-Kister model expresses the excess free energy of mixing as the sum of terms which consists of a function of the mole fractions of each component and an interaction parameter. In this study, the effect of added salts on the experimental enthalpy data (H^E) was correlated with H^E values calculated using the Redlich-Kister polynomial¹⁹.

$$H^E / [\text{J} \cdot \text{mol}^{-1}] = x_1 x_2 \sum_{i=0}^j A_i (2x_1 - 1)^i \quad (1)$$

where H^E is the enthalpy of mixing; x_1 and x_2 are the mole fractions of the solvents 1 and 2, respectively; and A_i is a constant that is a function of temperature and the system properties.

The experimental H^E values were fitted with Eq. (1) by the least-squares method with each point weighted equally, and the binary parameters (A_i) were evaluated. The modeling results are listed in Table 4 along with the percentage standard deviation ($\% \sigma(H^E)$). The values of the percentage standard deviation σ are computed from Eq. (2) and shown in Table 4.

$$\% \sigma(H^E) = \left[\frac{\sum \left(\frac{H^E_{\text{exptl}} - H^E_{\text{calcd}}}{H^E} \cdot 100 \right)^2}{(N - K)} \right]^{1/2} \quad (2)$$

where N and K are the number of data points and the number of parameters, respectively. The results obtained showed that the amount of the added salt has a strong effect on the estimated parameters and their corresponding standard deviations, which may have ensued from the interaction between the individual salt and the functional groups present in 2-propanol + acetic acid system.

CONCLUSION

From the experimental H^E and statistical data obtained in the present study using 2-propanol + acetic acid system, the salt NH_4Cl largely favored phase separation compared to ZnCl_2 by influencing the interaction between the weakly associated alcohol and the strongly associated acetic acid resulting in endothermic excess enthalpy values. The model represented the experimental data with the required

Table 4. The estimated parameters of equation (1) and the percentage of standard deviation $\% \sigma(H^E)$ of the system 2-propanol + acetic acid at 303.15 K

Salt conc. [wt.%]	A_0	A_1	A_2	A_3	$\% \sigma(H^E)$
no salt	6315.54	5478.73	-1323.18	194.59	1.96
5% ZnCl_2	5888.08	2016.96	5088.93	1656.00	1.44
10% ZnCl_2	6691.18	1068.62	1821.48	-4541.17	1.68
5% NH_4Cl	4860.99	-675.59	-1132.29	6670.05	1.89

accuracy for the studied system and therefore, this model is suitable to predict the excess enthalpy of mixing in 2-propanol + acetic acid binary mixture in the presence of the selected inorganic salts.

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