EEET ECOLOGICAL ENGINEERING & ENVIRONMENTAL TECHNOLOGY

Ecological Engineering & Environmental Technology 2023, 24(2), 55–66 https://doi.org/10.12912/27197050/157092 ISSN 2719-7050, License CC-BY 4.0 Received: 2022.11.05 Accepted: 2022.12.08 Published: 2023.01.01

Design of Artificial Neural Network for Prediction of Hydrogen Sulfide and Carbon Dioxide Concentrations in a Natural Gas Sweetening Plant

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ABSTRACT

Gas sweetening is a fundamental step in gas treatment processes for environmental and safety concerns. One of the most extensively used and largely recognized solvents for gas sweetening is methyl diethanolamine (MDEA). One of the most crucial metrics for measuring the effectiveness of gas treatment units is the amount of acid gas that has been treated with MDEA solution. As a result, it should be regularly monitored to avoid operational issues in downstream processes and excessive energy consumption. In this study, the artificial neural network (ANN) approach was followed to predict the H_2S and CO_2 sour gases concentrations of sweetening process. The model was built using dataset gathered from a real operation plant in Iraq, collected from February 2019 to February 2020, and used as input to the neural network. The data include H_2S and CO_2 concentrations of the feed gas, temperature, pressure, and flow rate of the unit. The designed ANN model showed good accuracy in modeling the process under investigation, even for a wide range of parameter variability. The testing outcomes demonstrated a high coefficient of determination (R^2) of greater than 0.99, while the overall training performance showed a low mean squared error (MSE) of less than 0.0003.

Keywords: natural gas dataset, ANN modeling, sour gases, absorption, sweetening process, MDEA.

INTRODUCTION

More than 40% of the world's natural gas reserves are very sour, containing substantial amounts of sulfur and CO_2 , increasing to 60% for Middle Eastern gas reserves (Al-Jadir and Siperstein 2019), Rafati 2019, Kadhim et al. 2021). Given that these gases can create corrosive acids that harm pipes, it is recommended that natural gas contain no more than two mol% carbon dioxide and four ppm hydrogen sulfide (Alqaheem 2021). If the hydrogen sulfide (H₂S) level of the natural gas surpasses 5.7 mg per cubic meter, the gas is typically regarded as soured Stewart and Arnold (2011). H_2S is a colorless, corrosive, water-soluble, highly toxic, and flammable acid gas that has the characteristic of the foul odor of rotten eggs (Georgiadis et al. 2020). One of the principal greenhouse gases, carbon dioxide (CO₂), accumulates continuously in the atmosphere and has a negative impact on the ecosystem, especially because of the global warming phenomena. Among many other industrial operations, CO₂ is emitted during the creation of electricity and the processing of natural gas.

Because of the harm that CO_2 , H_2S , and other NG contaminants may do to people, machinery, and the environment, these dangers are becoming

more and more concerning. You can categorize natural gas as sweet or sour. It contains nitrogen, CO_2 , O_2 , isopentane, n-pentane, hexane, and H_2 , as well as methane, ethane, propane, isobutene, and n-butane. Helium, hydrogen sulfide, and mercaptans are some additional gases that contribute to the gas' distinctive odor. The primary pollutants in NG are CO_2 and H_2S ; these pollutants can be captured using amine solvents, absorption apparatus, and membranes. By using the distillation and absorption processes, additional pollutants, such as carbonyl sulfide, mercaptans, ethane, pentane, etc., are often eliminated (Sanni et al. 2022).

Various gas-sweetening techniques must be used depending on the type and amount of acid gas impurities that need to be eliminated (Alardhi et al. 2022). The currently used processes are as follows: chemical absorption (Zhu et al. 2021), physical absorption (Burr and Lyddon 2008), membrane (Liu et al. 2020), direct conversion to sulphur (Mokhatab and Poe 2012), and physical adsorption (Webley 2014). Instead of relying solely on physical absorption, chemical reactions are mostly used to remove the acid gases from hydrocarbon gas mixtures (Seqatoleslami et al. 2011). Today, amine techniques are frequently employed to sweeten gas (Koolivand et al. 2011). To get rid of carbon dioxide and hydrogen sulfide, utilize amine solutions. The majority of onshore gas sweetening operations employ a method simply referred to as the "amine process." With this method, the gas containing hydrogen sulfide and/or carbon dioxide is pushed through a tower containing an amine solution. Similar to how glycol absorbs water, the amine solution is attracted to carbon dioxide and hydrogen sulfide. Diethanolamine and Monoethanolamine (MEA) are the two main amine solutions that are employed (DEA) (Stewart and Arnold 2011). A popular chemical absorbent used in refineries to remove acid gases is diethanolamine (DEA), which is classified as secondary, and methyl diethanolamine (MDEA), which is classified as tertiary. These solvents have several positive qualities, including low vapor pressure, low energy requirements, corrosiveness, high capacity, and high stability. Additionally, unlike DEA, MDEA is designed to remove H₂S selectively when the goal is to collect it in the presence of CO₂, whereas its reaction rate with CO_2 is minimal.

There are numerous limitations to traditional methods for chemical engineering challenges, such as nonlinear systems and modeling highly complex. However, in a number of real-world applications, artificial neural networks (ANN) have

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been shown to be capable of solving complex problems. Due to their capacity to somewhat mimic human problem-solving behavior, which is challenging to replicate utilizing the logical, analytical techniques of expert systems and conventional software technologies, ANNs represent one of the artificial intelligence paradigms that are currently undergoing the most rapid development. The flexibility and capacity of ANNs to simulate both linear and nonlinear systems without the need for an existing empirical model underlies their broad use. Due to this, the ANN has the edge over conventional fitting techniques in several chemical applications. The main objective of this research is to predict the concentration of sour gases and assessment the gas-sweetening process subject to different operating conditions. The ultimate goals of an assessment of the sour gas concentrations of the unit operating with a toxic gas are: (1) to satisfy the quality of the sweet gas, (2) to provide data that can be used to make decisions regarding safety measures and to ensure the environmentally safe release gas containing H₂S and CO₂. Furthermore, to protect workers and nearby residents. (3) Assessment of a toxic gas concentration release requires an evaluation of potential adverse health effects and an analysis of the hazard zone around the facility for different release scenarios. In this regard, the ANN will be used as a prediction tool to estimate H₂S and CO₂ concentrations after the natural gas sweetening process.

PROCESS FLOW AND DESCRIPTION OF PLANT

Sulfur removal and absorption of feed gas

The process flow is shown in Figure 1. The feed gas from the gas booster section enters this section under a temperature of 40–45°C and a pressure of 4.0 MPa. After the separation filter removes the small solid particles, the liquid droplets are still possibly entrained in the gas. The feed gas and the MDEA, with a percentage of 36–38 wt%, enter the amine absorption tower. The feed gas interacts with the amine solvent's lean solution as it moves from the bottom to the top of the unit. Lean amine inlets are provided on the 18th, 20th, and 24th tray layers of the main absorption tower for adjusting the absorber operation to adapt to the changes in feed gas quality and ensure the quality indexes of sweet wet gas. After the sweet wet



Figure 1. A schematic showing the use of an amine solvent during the sweetening process (Adib et al. 2013)

gas is separated from the liquid on the top of the main absorber by the sweet gas scrubber, it is then passed to the user.

Flashing of rich amine

The bottom of the amine absorber discharges the rich amine that has absorbed the acid gas. It enters the rich amine flash vessel after being pressure-adjusted by the liquid level control valve at the base of the absorption tower. The flash vessel's solution and the dissolved condensate in it are separated, and the condensate is skimmed out of the solution system. Flashing off the solution in the vessel causes some of the dissolved hydrocarbon gas to release. Most of the H_2S gas is separated from the flash gas as it flows from bottom to top and contacts the lean amine as it flows from top to bottom. The flash gas from the top of the flash vessel then goes to the low-pressure flare knockout drum.

Amine regeneration

Utilizing the liquid level control valve, the rich amine is pumped out of the depths of the rich amine flash vessel. Through the lean/rich solution heat exchanger, with the lean amine that is being delivered from the amine regenerator tower's base, it exchanges heat (HE), with its temperature rising to about 100 °C. After that, it enters the amine regenerator tower, flowing top to bottom and coming into touch with the steam, moving bottom to top inside the column in a count-current manner. This process allows the hydrocarbons, H_2S , and CO_2 to be removed from the rich solution. The lean amine is pumped to the amine

absorber (absorption tower), completing the circulation of the whole solution system. The regenerator reboiler provides the heat required by the regeneration. Acid gas goes into the Flare system or the Sulfur recovery unit. Hot lean amine goes out from the bottom of the amine regenerator. After its temperature is reduced to about 88 °C by exchanging heat with the rich amine in the lean/rich amine exchanger, it is sent to the amine gathering tank, which is then pumped by the hot lean amine pump to the lean amine air cooler. After cooling, part of the lean amine enters the lean amine filter to remove the mechanical impurities, then enter the activated carbon filter and lean amine solids filter for filtering and removing deterioration and degradation products from the solution. After filtering, the lean amine goes into the amine flash vessel and the amine recycling pump. The lean amine to the lean amine recycles pump is pumped to the absorption tower, completing the recycling of the whole solution system.

Chemical reactions and feed gas specification

Regarding the mass transfer rates, the reaction rates of H_2S with MDEA are practically immediate. Contrarily, compared to the rate of mass transfer of CO₂, the reaction rates of CO₂ with MDEA are limited and slow. The kinetic selectivity for H_2S is caused by this differential in reaction rates Pacheco and Rochelle (1998). The tertiary amine MDEA, having the chemical formula $(C_2H_4OH)_2NCH_3$, has a sluggish reaction with CO_2 but a nearly immediate reaction with H_2S . Principal process responses comprise:

• hydrogen sulfide and the reaction:

$$(C_2H_4OH)_2NCH_3 + H_2S \leftrightarrow$$

$$(C_2H_4OH)_2NCH_4^+ + HS$$
 (1)

• the reaction with carbon dioxide:

$$(C_{2}H_{4}OH)_{2}NCH_{3} + CO_{2} + H_{2}O \leftrightarrow (C_{2}H_{4}OH)_{2}NCH_{4}^{+} + HCO_{3}$$
(2)

However, the above two reactions are reversible. Moreover, Table 1 gives the composition of the natural gas obtained using gas chromatography.

ISSUES WITH GAS SWEETENING PLANTS

Gas sweetening units have numerous issues, some of which are brought on by inadequate knowledge of the relevant process parameters. With the aid of artificial neural network models, the problems can be predicted. Following is a list of some problems brought on by rich amine conditions: Gas is not sweet, dirty degraded amine, excessive energy consumption, and excessive corrosion Rahmanpour et al. (2015).

MODELING USING ARTIFICIAL NEURAL NETWORKS

One of the artificial intelligence methods, known as an artificial neural network (ANN), was inspired by the neural networks in the human nervous system (Agwu et al. 2020). Since the 1980s, artificial intelligence research has greatly benefited from the use of neural networks, which have several applications in data processing, classification, performance approximation, and numerical control (Ram et al. 2019). Similar to how synapses interact in the brain, nodes in such networks' mathematical structures stand in for neurons and layers for their interconnected layers. Since their conception, ANNs have been widely accepted, yet, as computing power increased, ANNs began to earn more notoriety. This use has aided the ANN algorithms' scientific advancement, which began with single-layer perceptrons before switching to multilayer perceptrons; after that, the backpropagation algorithm was introduced, which led to many new types of ANNs (Anagnostis et al. 2020).

Data collection

A good performance of the sweetening unit depends on the proper optimization of operating parameters (Pandey 2005). In this regard,

Table 1. Standard for	feed	gas	gathered	from	а	real
operation plant in Iraq						

Component	Feed gas specification (mole %)		
Nitrogen / Oxygen (N ₂ /O ₂)	0.838215		
Carbon dioxide (CO ₂)	5.334857		
Hydrogen sulfide (H ₂ S)	2.2		
Methane (C1)	62.583378		
Ethane (C2)	15.201929		
Propane (C3)	8.210851		
Iso Butane (I-C4)	1.067931		
Normal Butane (N-C4)	2.86071		
Neo Pentane (NEO-C5)	0.003401		
Iso Pentane (I-C5)	0.758717		
Normal Pentane (N-C5)	0.000696		
Total Hexane (Total C6)	0.0758543		
Total Heptane (Total C7)	0.043142		
Total Octane (Total C8)	0.028211		
Total Nonane (Total C9)	0.000907		
Total Decane (Total C10)	0.000419		
Total	100		

five input key process parameters, H_2S and CO_2 concentrations, temperature, pressure, and flow rate of input gases data, were collected from a local refinery in Iraq over a one-year period. The raw dataset from this system consists of 243 data points sampled from February 2019 to February 2020. The considered output parameters are H_2S and CO_2 concentrations after the gas sweetening process. The minimum and maximum values of each parameter and the units of measurement are shown in Table 2. The plant can process sour gas with 1.2 MMTPA of aromatics with eight trains of natural gas sweetening units (41 MMSCF/D). It has absorption and stripping towers and uses MDEA as a solvent.

Normalization and Implementation of ANN

Due to the slightly disparate scales of the different variables in the dataset, a min-max normalization approach was applied to the training data to bring all features to the same scale. Normalization is a crucial step in the control of bias in linear regression modeling. Regardless of how important a variable is to the prediction, if the scales of the two variables are substantially different, the regression analysis will be more heavily influenced by the item with the larger scale (Chawade et al. 2014, Al Jarrah 2022). Using Equation 3, the data were

Process Parameters		Mini	mum	Maximum		
		H ₂ S	CO ₂	H ₂ S CO ₂		
Inputs	Concentrations	12200 ppm	0.04 %	26600 ppm	4.72%	
	Temperature (ºC)	13.5		48		
	Pressure (MPa)	0.37		2.15		
	Flow rate of input gases (MMSCF/D)	7.34		37.9		
Outputs	Concentrations	0.04 ppm	0.04 %	9.5 ppm	4.72%	

Table 2. The process input and output parameters

scaled and normalized to fit the transfer function in the hidden (i.e., sigmoid) and output layers (i.e., linear) (Rene et al. 2013).

$$\widehat{X} = \frac{X - X_{min}}{X_{max} - X_{min}} \tag{3}$$

where: \hat{X} – the normalized value; X_{min} and X_{min} are the minimum and maximum values of X, respectively (Al Jarrah 2022).

In this paper, the neural network toolbox of MATLAB software was used to predict the H_2S and CO_2 concentrations of the gas sweetening process. Table 3 lists the parameters selected for the ANN model. The models were trained and tested using the dataset defining the procedure. In order to minimize the loss, expressed as the Mean Squared Error (MSE) between predictions and actual values, the training objective was to identify the model's internal parameters. Equation 4 was applied to the MSE calculations. Before starting the program, the dataset was loaded, shuffled, and split into training (70% of the dataset), validation (15% of the dataset).

$$MSE = \frac{1}{n} \sum_{i=1}^{n} \left(Out_{experimental} - Out_{predicted} \right)^2 \quad (4)$$

Table 3. Parameter settings for the ANN model

where: n – the number of data sets for which the MSE is computed, $Out_{experimental}$ – the value of the analyzed parameter obtained from the experimental work, $Out_{predicted}$ – the ANN predicted value.

The number of hidden layers ranged from one to six hidden layers, and it is observed that increasing the number of hidden layers improves the accuracy of the model prediction. However, it increases the computation time for learning drastically.

Framework of ANN

The current study used the ANN approach to forecast the output parameters (H_2S and CO_2 concentrations) based on how input parameters operate (temperature, pressure, flow rate, H_2S , and CO_2 concentrations). Figure 2 displays the multilayer feed-forward artificial neural network's created configuration.

Determining a training algorithm to utilize is the first step in creating the neural network model. Because it enables the network to adopt, the

Daramatara	Values		
Parameters	H ₂ S	CO ₂	
Training data set	171		
Testing data set	36		
Validation data set	36		
Number of hidden layers	1,2,3,4,5, and 6		
Number of neurons in the hidden layer	5, 10,15, 20, 25, 30, 35, and 40		
Activation function (hidden layer)	Tansig		
Activation function (output layer)	Purelin		
Number of epochs	1000		
Learning rate	0.7		
Architecture selection	Trial-and-error		
Target goal mean square error	0.0003		

backpropagation network – a potent multilayer, feed-forward neural network was used in the current study. They can train a network on a common set of input/output pairs and get good results without training the network on all possible input/ output pairs thanks to the backpropagation network's generalization characteristic. One or more hidden layers of sigmoid neurons, followed by an output layer of linear neurons, are common components in feed-forward networks. The network can learn both linear and nonlinear relationships between input and output vectors thanks to its multiple layers of nonlinear transfer function neurons. In contrast to the desired output, as shown during the training phase, Figure 3 displays the network's actual output. As a result, the network's weights were updated by propagating the resulting error backward. The proposed intelligent network can be utilized to provide an alternative method to predict the H₂S and CO₂ concentrations of the sweeting process.

Additionally, this intelligent approach predicts more quickly than traditional simulation parameters or even mathematical methods. As shown in Figure 4, the intelligent system is prepared to anticipate performance after training based on the learned learning parameters that have been saved. The training method normally consists of steps: (1) build the network object after putting together the training data; (2) prepare your network; (3) model the network's reaction to fresh inputs. The steps that must be taken to build a suitable network are shown in Figure 5.

RESULTS AND DISCUSSION

Function, number of neurons, and hidden layers for optimal training

In MATLAB, the ANN toolbox has different backpropagation training algorithms. The feed-forward learning strategy is utilized in conjunction with quick processing algorithms, such as TRAINBR, TRAINBFG, TRAINOSS, and TRAINLM, as a technique for numerical optimization. The MSE and R^2 were used to compare. With the testing data, it was discovered that the training function TRAINLM produces the best results. The TRAINLM algorithm is an iterative technique for finding the minimum of a multivariate error function, expressed as the sum of squares of the difference between the actual and target outputs.

An ANN is made up of hundreds of single units, also known as artificial neurons or processing elements, which are linked together by coefficients (weights) to construct the layers that



Figure 2. An artificial neural network with multiple layers that are configured



Figure 3. The intelligent system's initial training phase



Figure 4. The intelligent system's testing phase

make up the neural structure. The interconnection of the neurons in a network is what gives brain calculations of their capacity. The accuracy of the prediction produced depends on how well the neurons are interconnected in the networks. The transfer functions of a neural network's neurons, the learning rule, and the architecture itself all affect how active it is. Another illustration of a hidden layer in an ANN design is the layer that sits between the input and output layers. Therefore, the most important variables influencing predictive performance are the number of hidden layers and the number of neurons in each hidden layer. Most of the previous studies did not propose any criteria to find out the optimal number of neurons and hidden layers. The purpose of this study was to elucidate the significance of the number of neurons and hidden layers by addressing this topic. The size of neurons has changed thanks to the established



Figure 5. Flowchart summarizing the steps applied





ANN model (i.e., 5, 10, 15, 20, 25, 30, 35, and 40). Additionally, the quantity of concealed layers has altered (i.e., 1 to 6). In ANN models, we adjusted the neurons and hidden layers until the performance was optimal. Figure 6 highlights the outcomes of trial and error to establish the ideal number of neurons. Where the number of hidden layers is changed gradually from 1 to six hidden layers. Hence, the results show that increasing the number of hidden layers reduces the MSE by increasing the time response of the training process. Moreover, the optimum number of neurons in the hidden layer affects the performance. It is apparent that increasing the number of neurons reduces the MSE. However, increasing the number of neurons to more than 15 will not affect the performance in the degree of increasing the time, as illustrated in Figure 7. Moreover, the performance of selecting the optimum number of the learning algorithm is crucial to improve the prediction process during testing. Moreover, the optimal ANN architecture for H₂S and CO_2 in this study is presented in Figure 8.

The ANN model's effectiveness

Figure 9 shows the outcome of the training performance of the objective (H_2S and CO_2 concentrations) with the mean square error and the quantity of training network epochs. Once the lowest errors in the testing and verification curves

are almost identical based on the epoch numbers, the training is considered successful. As shown in Figure 9, the result of the H₂S concentration of sweetening gas converged to a mean square error of 2.0023e-06 at the 252-iteration for the 5-15-2 network architecture. Because of its greater ability to forecast outcomes for the aim of the gas sweetening process, the 5-15-2 design is therefore regarded as the ideal neural network for the current challenge (H₂S and CO₂ concentrations). In addition, a comprehensive comparison to choose the best learning algorithm has been accomplished, and this study shows that the Levenberg Marquardt algorithm act perfectly during the training phase compared to other learning algorithms, as shown in Figure 10. According to indications, the training results meet the following requirements: The testing curve and verification curve are not substantially dissimilar from one another, the mean square error is low, and there was minimal overfitting during the training phase. Moreover, Figure 11 shows the scatter plots of ANN predicted output sour gases concentrations (H₂S and CO₂) of the actual data obtained from the gas sweetening plant for the training, testing, and validation sets, and, generally, the overall model, respectively. The value is close to 100 percent, which shows that the artificial neural network method used to create the prediction model performed very well.



Figure 7. Optimization of the training function, number of layers, and the hidden neurons of each architecture used to model and predict H₂S and CO₂ concentrations



Figure 8. The obtained optimum structure of ANN architecture for prediction of H₂S and CO₂ output concentrations



Figure 9. Performance of trained network for prediction of H₂S and CO₂ output concentrations



Figure 10. Comparison between different learning algorithms (a) MSE and (b) R^2



Figure 11. Scatter plots of the developed ANN model of H₂S and CO₂ output concentrations

CONCLUSIONS

Because of the advantages to the environment, natural gas, which is now one of the major energy carriers, will play a larger role among energy sources in the future. The amine sweetening plant of a case study refinery was simulated by ANN, and a model was used to simulate the absorption process. The model was validated through actual industrial data, and results showed that the model had high accuracy. This study demonstrates how ANN may be used to create precise prediction models for the operational variables of a natural gas sweetening plant for industrial use. In addition to the basic benefits indicated for ANN as an input/output modeling tool, the projected data in this study demonstrated good accuracy performance from artificial neural networks. The developed

ANN model was constructed using the best possible architecture, which included: 5-15-2 architecture is considered the best neural network with one hidden layer for the specified architecture. The R² was higher than 0.99 in the testing results, and the entire training had a low MSE of less than 0.0003, proving that ANN models can successfully predict the amounts of sour gases in a natural gas sweetening facility. The pace of learning and prediction could be increased by integrating the generated ANN model with other optimization methods.

REFERENCES

 Anagnostis A.P., Elpiniki, B., Dionysis. 2020. Application of Artificial Neural Networks for Natural Gas Consumption Forecasting. Sustainability, 12, 6409.

- Al Jarrah A. 2022. Using Jordanian Natural Zeolite for Capturing Hydrogen Sulfide Gas. Ecological Engineering & Environmental Technology, 23(5), 164–168.
- Al Jarrah A.M. 2022. Using Jordanian Natural Zeolite for Capturing Hydrogen Sulfide Gas. Ecological Engineering & Environmental Technology, 23(5), 164–168.
- Alardhi S., Jabbar N., AL-Jadir T., Ibrahim N. K., Dakhil A.M., Al-Saedi N.Dh., Al-Saedi H. Dh., Adnan M. 2022. Artificial neural network model for predicting the desulfurization efficiency of Al-Ahdab crude oil, AIP Conference Proceedings, 2443, 030033.
- Al-Jadir T., Siperstein F.R. 2019. Modeling and simulation of adsorption of methane, ethane, hydrogen sulfide and water from natural gas in (FP)YEu Metal–Organic Framework. IOP Conference Series: Materials Science and Engineering, 579, 012020.
- Alqaheem Y. 2021. A simulation study for the treatment of Kuwait sour gas by membranes. Heliyon, 7, e05953.
- 7. Burr B., Lyddon L.G. 2008. A Comparison of Physical Solvents for Acid Gas Removal.
- Georgiadis A., Charisiou N. D., Goula M. A. 2020. Removal of Hydrogen Sulfide from Various Industrial Gases: A Review of The Most Promising Adsorbing Materials. Catalysts, 10, 521.
- Kadhim W., Al-Jadir T., Albrazanjy M.G., Al-Rubaiey N.A., Mohammed Dakhil A., Al-Saedi N.D., Rahima M.H.A. 2021. Sulphide pollutants elimination and degradation in petroleum wastewater by ozonation process. IOP Conference Series: Earth and Environmental Science, 779, 012086.
- Koolivand Salooki M., Abedini R., Adib H., Koolivand H. 2011. Design of neural network for manipulating gas refinery sweetening regenerator column outputs', Separation and Purification Technology, 82, 1–9.
- Liu Y., Liu Z., Morisato A., Bhuwania N., Chinn D., Koros W.J. 2020. Natural gas sweetening using a cellulose triacetate hollow fiber membrane illustrating controlled plasticization benefits. Journal of Membrane Science, 601, 117910.
- Mokhatab S., Poe W.A. 2012. Handbook of Natural Gas Transmission and Processing. Gulf Professional Publishing: Boston.
- 13. Okorie A., Akpabio J.U., Dosunmu A. 2020. Artificial neural network model for predicting the density of oil-based muds in high-temperature,

high-pressure wells. Journal of Petroleum Exploration and Production Technology, 10, 1081–1095.

- Pacheco M., Rochelle G.T. 1998. Rate-Based Modeling of Reactive Absorption of CO₂ and H₂S into Aqueous Methyldiethanolamine. Industrial & Engineering Chemistry Research, 37, 4107–4117.
- Pandey M. 2005. Process Optimization in Gas Sweetening Unit – A Case Study. In International Petroleum Technology Conference.
- 16. Rafati N. 2019. A Novel Low-Cost Process for Sour Gas Sweetening and NGL Recovery. In Abu Dhabi International Petroleum Exhibition & Conference.
- 17. Rahmanpour O., Zargari M.H., Ghayyem M.A. 2015. Application of Artificial Neural Networks (ANNs) to Predict the Rich Amine Concentration in Gas Sweetening Processing Units. Energy Sources, Part A: Recovery, Utilization, and Environmental Effects, 37, 118–126.
- Ram M., Taklif A., Faridzad A. 2019. Prediction of Natural Gas Prices in European Gas Hubs Using Artificial Neural Network. Petroleum Business Review, 3, 1–14.
- 19. Rene E. Estefanía López M., Hoon Kim J., Suck Park H. 2013. Back Propagation Neural Network Model for Predicting the Performance of Immobilized Cell Biofilters Handling Gas-Phase Hydrogen Sulphide and Ammonia. BioMed Research International, 463401.
- 20. Sanni S., Agboola O., Fagbiele O., Ojima Yusuf E., Eterigho Emetere M. 2020. Optimization of natural gas treatment for the removal of CO₂ and H₂S in a novel alkaline-DEA hybrid scrubber. Egyptian Journal of Petroleum, 29, 83–94.
- Seqatoleslami N. KoolivandSalooki M. Mohamadi N. 2011. A neural network for the gas sweetening absorption column using genetic algorithm. Pet. Sci. Technol., 29, 1437–1448.
- 22. Stewart M., Arnold K. 2011. Gas Sweetening and Processing Field Manual, Gulf Professional Publishing: Boston.
- Webley P. 2014. Adsorption technology for CO₂ separation and capture: a perspective. Adsorption, 20, 225–231.
- 24. Zhu W., Ye H., Zou X., Yang Y., Dong H. 2021. Analysis and optimization for chemical absorption of H₂S/CO₂ system: Applied in a multiple gas feeds sweetening process', Separation and Purification Technology, 276, 119301.